

1 Microalgae grow on source separated human urine in Nordic climate: 2 outdoor pilot-scale cultivation

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12 Abstract

13 Human urine contributes approximately 80% of nitrogen and 50% of phosphorous in urban
14 wastewaters while having a volume of only 1 - 1.5 L/d per capita compared to 150 - 200 L/d
15 per capita of wastewater generated. There is interest to study source separation of urine and
16 search methods to recover the nutrients form the urine. In this study, the objective was to use
17 the nutrients in source separated urine for outdoor cultivation of microalgae in Nordic climate.
18 A freshwater green microalga *Scenedesmus acuminatus* was grown in different dilutions (1:20
19 and 1:15) of source separated human urine, in a semi-continuously operated outdoor raceway
20 pond with a liquid volume of 2000 L, at hydraulic retention time of 15 d. The microalgae could
21 remove 52% nitrogen and 38% phosphorus even at culture temperatures as low as 5 °C, while
22 obtaining a biomass density of 0.34 g VSS/L. Harvested microalgal biomass could be used to
23 produce methane with a yield of 285 L CH₄/kg volatile solids.

24 **Keywords:** Microalgae, nutrient recovery, raceway pond, *Scenedesmus acuminatus*, source
25 separated human urine

26 1. Introduction

27 Municipal wastewaters are increasingly treated in centralized wastewater treatment units i.e. in
28 one single treatment unit for one or a group of cities (Massoud et al., 2009). The sewers carry
29 large volume of diluted wastewater in long pipelines involving large quantity of excavation
30 and energy for pumping (Massoud et al., 2009; Suriyachan et al., 2012). About 80-90% of the

31 capital costs for centralized wastewater treatment systems are related to the collection system
32 with potential economies of scale associated to densely populated areas (Maurer et al., 2005).
33 On the other hand, decentralized treatment system can be defined as treatment units where the
34 raw wastewater is collected, treated, disposed and reused close to its source (Massoud et al.,
35 2009). Decentralized treatment systems configured with large cluster subsystems (population
36 > 2000) was estimated to be cheaper than centralized wastewater treatment (population around
37 30000), with lower operation and maintenance requirement, but with higher capital cost (Jung
38 et al., 2018).

39 Approximately 80% of nitrogen, 50% of phosphorous and 90% of potassium in domestic
40 wastewater originate from human urine, depending on diet and lifestyle, use of detergents etc.
41 (Chang et al., 2013). However, the production volume of urine is only 1 – 1.5 L per person per
42 day (Chang et al., 2013), while the total wastewater discharge may be up to 150 - 250 L/d. In
43 addition to large amount of N, P and K, human urine also contains trace elements like B, Cu,
44 Zn, Mo, Fe, Co and Mn. Nitrogen and phosphorus are only partially captured in a reusable
45 form in conventional centralized wastewater treatment systems. The development of urine
46 sorting toilets has made it possible to separate urine for nutrient recovery instead of directing
47 the urine to centralized wastewater treatment plants (Adamsson, 2000; Igos et al., 2017).

48 Several methods have been studied to capture the nutrients from source separated urine, such
49 as struvite precipitation (Wilsenach et al., 2007), ion exchange (Lind et al., 2000), and ammonia
50 stripping (Başakçılardan-Kabakci et al., 2007). However, nitrogen recovery is rather low in
51 struvite precipitation along with the need for addition of magnesium, and ammonia stripping
52 demands additional energy. Microalgae, if grown on urine, may provide an economically and
53 environmentally sustainable way to capture nutrients from urine as nutrients are utilized by the
54 growing microalgal cells (Feng and Wu, 2006). *Scenedesmus* species, for example, have been
55 reported to take up high concentrations of nitrogen and phosphorus ($\text{NH}_3\text{-N} = 273 \text{ mg L}^{-1}$, total
56 $\text{P} = 58.75 \text{ mg L}^{-1}$) (Kim et al., 2015). Choi and Lee (2015) have reported that *Scenedesmus* can
57 grow in different media with the N/P ratio varying over a wide range of 5 to 30. .

58 Azov and Goldman (1982) demonstrated that the photosynthesis rates of *Scenedesmus* are
59 reduced to 50% of their maximum rates when free ammonia reached 20 mg/L. Thus, dilution
60 of human urine is considered necessary to reduce the toxic effect of the high ammonia
61 concentration on the growth of microalgae. The growth of different microalgae in diluted
62 human urine has previously been studied using cyanobacterium *Spirulina platensis* (Feng and

63 Wu, 2006) and microalga *Chlorella vulgaris* (Jaatinen et al., 2016), *Chlorella sorokiniana*
64 (Tuantet et al., 2014) and *Scenedesmus acuminatus* (Adamsson, 2000). *Scenedesmus* has been
65 reported to grow in 0.5% diluted urine supplemented with EDTA and iron up to a maximum
66 biomass density around 133 mg/L as dry weight (Adamsson, 2000). However, there are no
67 published studies on large scale outdoor cultivations of *Scenedesmus* or other microalgae in
68 Nordic climate conditions with varying lengths of daylight from 23 hours to 1 hour and outside
69 temperatures ranging from -30 to 30 °C.

70 Large-scale cultivation of microalgae in human urine would create a sink for nutrients.
71 Eventually, to close the nutrient cycle, proper end use of the microalgal biomass needs to be
72 envisaged. Use of microalgae as biofuel, nutraceutical (pharmaceutical grade nutrients), or high
73 value chemicals is getting increasing attention (for reviews and discussion see, Kim et al., 2016;
74 Passos et al., 2014). While majority of the biofuel production processes from microalgae
75 requires the costly steps of drying, extraction and fuel conversion, in anaerobic digestion (AD)
76 a natural consortium of microorganisms is able to break down the organic matter of the algal
77 biomass into simple monomers which can then be converted into biogas (Abdelaziz et al.,
78 2013). In addition to the produced biogas, nutrients in the substrate are retained in the AD
79 digestate, which can be further refined as fertilizers or circulated back to algae cultivation
80 (Kinnunen et al., 2014). Varying biochemical methane potential (BMP) between 107 and 410
81 L CH₄ kg⁻¹ volatile solids have been found for *Scenedesmus* dominating biomass, mainly
82 cultivated in different synthetic media or wastewater and the BMP has been reported to vary
83 depending on the growth media (Frigon et al., 2013; Kinnunen and Rintala, 2016; Roberts et
84 al., 2016; Zhen et al., 2016).

85 City of Tampere in Finland is building a new city district in Hiedanranta that serves as an
86 experimental living lab and promotes circular economy. In Hiedanranta, the city will proceed
87 e.g. with the approach of decentralization, focusing on recovery of resources from wastewater
88 generated in the area locally. In this study, the feasibility to cultivate microalga *Scenedesmus*
89 *acuminatus* using source separated and hydrolyzed (stored for several months to kill the
90 pathogens, while urea is hydrolyzed) human urine was studied in pilot scale outdoor raceway
91 ponds in Hiedanranta. The requirements for diluting the urine for algal growth were determined
92 both in laboratory- and pilot-scale. In addition, the biochemical methane production potential
93 of the microalgal biomass harvested from the pilot-scale ponds was tested. To our knowledge,
94 cultivation of microalgae in pilot-scale outdoor raceway pond to treat real human urine in
95 Nordic climate has not been previously reported.

96 **2. Materials and methods**

97 *2.1. Laboratory cultivation of Scenedesmus acuminatus*

98 *Scenedesmus acuminatus* (SAG 38.81) was obtained from the Culture Collection of Algae
99 (SAG) at the University of Göttingen, Germany. The stock culture was maintained under
100 continuous fluorescence illumination of 40 $\mu\text{mol photons/m}^2\cdot\text{s}^1$ in 700 mL modified N8
101 medium with the following composition (per liter): 0.5055 g KNO_3 ; 0.74 g KH_2PO_4 ; 0.2598 g
102 Na_2HPO_4 ; 0.05 g $\text{MgSO}_4 \times 7\text{H}_2\text{O}$; 0.0175 g $\text{CaCl}_2 \times 2\text{H}_2\text{O}$; 0.0115 g $\text{FeNaEDTA} \times 3\text{H}_2\text{O}$;
103 0.0032 g $\text{ZnSO}_4 \times 7\text{H}_2\text{O}$; 0.013 g $\text{MnCl}_2 \times 4\text{H}_2\text{O}$; 0.0183 g $\text{CuSO}_4 \times 5\text{H}_2\text{O}$ and 0.007 g
104 $\text{Al}_2(\text{SO}_4)_3 \times 18\text{H}_2\text{O}$ at a pH of 8.5. The media was continuously purged with 5% CO_2 in air at
105 a flow rates of 0.2 L/min. The initial optical density (OD_{660}) of the culture was 0.5. When the
106 OD_{660} reached the value of 5.5 – 5.8 (growth saturation), 5 mL of cells washed with distilled
107 water were inoculated into 700 mL of fresh medium and the saturated culture was finally stored
108 in the dark at 8 °C (used as inoculum in further studies).

109 *2.2. Source separated urine collection and storage*

110 The source separated urine (later referred to as urine) was collected from the experimental
111 cultural and seminar center in Hiedanranta (Tampere, Finland) by using urine diverting dry
112 toilets, which were being used by the visitors of the center. The urine was collected in 1000 L
113 plastic tanks and stored for at least six months at ambient temperature (5 - 20 °C) before use to
114 kill the pathogens and hydrolyze the urea. The composition of the urine after storage (as
115 average for the different samples collected over the period of operation of the ponds) was as
116 presented in Table 1.

117

118 Table 1. Average composition (and standard deviation) of urine (five samples) after storage for
119 at least six months at ambient temperature

Parameter	Range
pH	8.8 ± 0.0
COD (mg/L)	5500 ± 200
N _{tot} (mg/L)	3480 ± 130
NH ₄ ⁺ -N (mg/L)	1800 ± 750
P _{tot} (mg/L)	190 ± 52
Na (mg/L)	690 ± 30
K (mg/L)	600 ± 38
Mg (mg/L)	2.3 ± 0.4
Ca (mg/L)	14 ± 5

120 COD – chemical oxygen demand,

121 2.3. Screening for different dilutions of urine as growth medium

122 Source separated urine (Table 1) to be used as growth medium for *S. acuminatus* was diluted
123 with tap water to obtain the following dilutions: 0x, 2x, 3x, 4x, 5x, 10x, 15x, 20x and 25x. Here
124 2x dilution means 50% (v/v) urine in tap water and 25x means 4% urine in tap water. Duplicate
125 cultures with 5 mL of *S. acuminatus* stock culture was inoculated to 100 mL of growth medium
126 at each dilution in 250 ml Erlenmeyer flasks. The cultivations were incubated at 25 °C at 150
127 rpm and under continuous illumination with white fluorescent lamps at 40 μmol/m².s⁻¹ for seven
128 days. The growth of *S. acuminatus* was followed by analyzing OD₆₆₀ every day.

129 2.4. Cultivation of microalgae in raceway ponds

130 Two raceway ponds (RwP), used for cultivation of microalgae on human urine, were located
131 near to the collection site of the human urine in Hiedanranta (Tampere, Finland) inside a
132 greenhouse (Fig. S1). The small raceway pond (SRwP; L:W:D of 3 m: 0.5 m: 0.4 m) and the
133 big raceway pond (BRwP; L:W:D of 7 m: 1 m: 0.6 m) had liquid volumes of approximately
134 400 L and 2000 L, respectively. The ponds were constructed with gravel and lined with a 1.5
135 mm thick high-density polyethylene sheet. To maintain a constant velocity of liquid, the ponds
136 were equipped with paddle wheels (rotation speed of 10 rpm) operated with a 0.5 HP gear
137 wheel motor (Regal Beloit, Marathon motors, USA).

138 The SRwP was inoculated with 10 L of *S. acuminatus* (approximate OD₆₆₀ of 0.5), grown in
139 modified N8 medium and was operated as batch with 20x diluted urine. After 10 days,
140 approximately 350 L of the culture (OD₆₆₀ of 0.75) was used as inoculum for the BRwP which
141 was filled with 20x diluted urine to reach a total volume of 2000 L. The rest of the SRwP
142 culture (50 L) was used as inoculum for batch operation in the smaller pond, which was
143 operated to study the maximum growth of *S. acuminatus* in 20x urine and also to act as a culture
144 reserve. The level of medium in the SRwP was maintained constant by adding fresh water
145 weekly (approximately 10 L) to account for the evaporation loss.

146 After operation in batch mode for the first 15 days, the BRwP was operated in a semi-
147 continuous mode at a hydraulic retention time (HRT) of 15 d with 20x diluted urine for 28
148 days, after which the urine dilution was changed to 15x. After day 79, the BRwP was operated
149 in batch mode up to day 148, when the pond operation was stopped due to decrease in
150 temperature and light intensity.

151 The BRwP was fed two times a week by removing 500 L of the culture and replacing it with
152 20x (25 L of urine and 475 L of tap water) or 15x (33 L of urine and 467 L of water) diluted
153 urine. Two samples were collected during each feeding, one before and one 15 min after the
154 feeding. Before each feeding, 500 L of microalgal culture was collected in a drainage pit with
155 an attached nylon filter cloth (pore size < 10 µm). The microalgal biomass was recovered from
156 the cloth and a composite sample (500 mL) of the filtered water was collected. Harvested
157 biomass was centrifuged for 2 min at 4000 rpm, at 20°C. Settled algal pellets were washed with
158 deionized water, centrifuged (2 min, 4000 rpm, 20 °C) and either freeze-dried (CHRIST, Alpha
159 1-4 LD, Germany) for at least 17 h or stored as such at -20 °C.

160 *2.5. Methane production potential*

161 Methane production potentials of the harvested biomass was determined in triplicate batch
162 assays using 119 mL glass serum bottles. Methane production assays were done with biomass
163 collected from different phases of growth in BRwP namely 20x dilution phase (healthy cell
164 growth, day 25), 15x dilution start phase (cells were dying, day 32), 15x dilution stable phase
165 (freeze dried, day 53 and stored as such, day 79). Inoculum used in the tests was digestate from
166 a mesophilic anaerobic digester treating municipal wastewater treatment plant sludge
167 (Viinikanlahti, Tampere, Finland). Inoculum (30 mL) and microalgal biomass as the substrate
168 were added into the bottles, using a VS_{substrate}: VS_{inoculum} ratio of 1:1 (volatile solids, VS).
169 Distilled water was added to make a total liquid volume of 60 mL, and 4 g/L NaHCO₃ was

170 added as buffer. Inoculum alone with distilled water and buffer to make a total volume of 60
171 mL was used as control (three replicates) and the methane volume produced in the control was
172 subtracted from the methane volumes obtained in the bottles with the substrates. The bottles
173 were flushed with nitrogen gas for 1 min and sealed gas tight with rubber stoppers and
174 aluminum seals. The cultures were incubated at 35 °C without mixing.

175 *2.6. Analysis and calculations*

176 Light intensity and temperature of culture media in the ponds was measured every working
177 day. Culture suspension samples were collected from the raceway ponds every working day
178 and the effluent after harvesting was collected twice a week. The culture suspension samples
179 were analyzed for OD, pH, dissolved oxygen (DO), total suspended solids (TSS), volatile
180 suspended solids (VSS), total chemical oxygen demand (TCOD), soluble COD (SCOD), total
181 soluble phosphorus (P_{tot}), total soluble nitrogen (N_{tot}), ammonia nitrogen ($\text{NH}_4^+\text{-N}$) and other
182 cations namely potassium, magnesium, calcium and sodium. While TCOD is the COD of the
183 entire sample, the SCOD was measured after filtration with 0.45 μm syringe filter.

184 The pH and dissolved oxygen (DO) were measured using pH electrode and DO probe (HACH
185 Lange, HQ40D, U.S). Algal growth for all experiments was monitored by measuring optical
186 density at 660 nm (OD_{660}) using UV-VIS spectrophotometer (Shimadzu UV-1700
187 PharmaSpec). Additional monitoring of algal growth and health was conducted using bright-
188 field microscope (Axio-Imager, Carl Zeiss, Germany) and the samples were photographed
189 using an AxioCam HRc CCD camera equipped with AxioVision software (Carl Zeiss,
190 Germany). Total suspended solids (TSS) and volatile suspended solids (VSS) were analyzed
191 according to the Standard Methods (APHA, 1998). P_{tot} , N_{tot} and $\text{NH}_4^+\text{-N}$ were determined with
192 HACH Lange kits (LCK 350, LCK 303, and LCK 304) according to the protocols provided by
193 the manufacturer (HACH, 2017) after filtration with 0.45 μm syringe filter. Cations in the
194 sample were analyzed according to the ion chromatography standard SFS-EN ISO 10304-1
195 using an ion chromatograph (Dionex DX-120, USA) with AS40 autosampler, IonPac CS12A
196 cation exchange column and CSRS 300 suppressor (4 mm). The eluent contained 2 mM
197 methane sulphonic acid and the eluent flow rate was 1 mL min^{-1} . COD was analyzed with
198 dichromate method according to the Finnish Standard (Standard SFS 5504). Total COD
199 (TCOD) was analyzed from source separated urine, and soluble COD (SCOD), after filtration
200 with 0.45 μm syringe filter, was analyzed from the effluent after collection of the algal biomass.

201 The harvesting efficiency was calculated using Eq. 1:

202 $Efficiency = \frac{VSS_{inlet} - VSS_{outlet}}{VSS_{inlet}} * 100\%$ Eq. 1

203 where VSS_{inlet} is the VSS of the culture in the semi-continuous pond and VSS_{outlet} is the VSS
204 of the effluent after biomass harvesting.

205 Nutrients balance in the pond was calculated according to Eq. 2 and Eq. 3:

206 $Inflow = Assimilation + Precipitation + Volatilization + Outflow$ Eq. 2

207 $Removal (\%) = \frac{Assimilation + Precipitation + Volatilization}{Inflow}$ Eq. 3

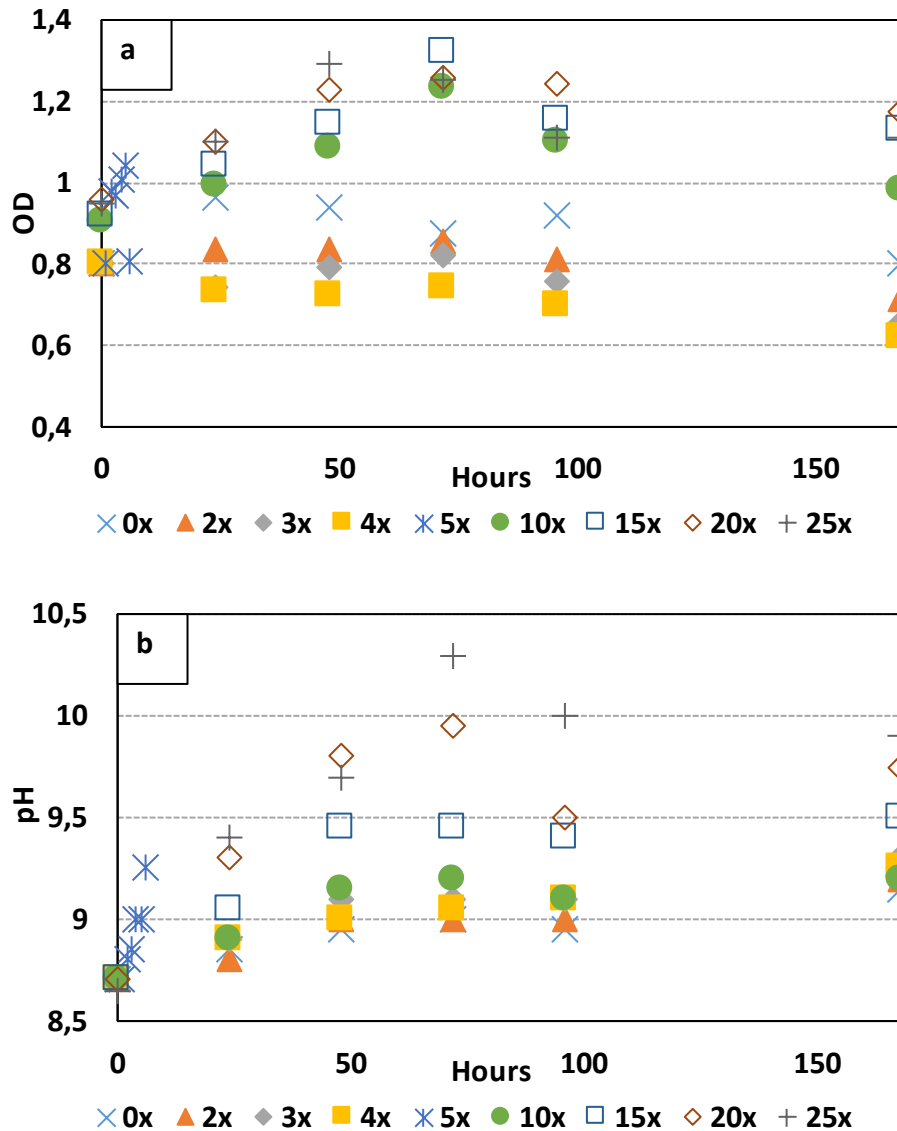
208 where, concentration of a specific nutrient in the inflow was measured from the fed urine
209 samples. The pond was considered to have completely mixed conditions, so outflow sample
210 was assumed to be representative of the pond contents. The sum of assimilation to the biomass,
211 precipitation and volatalization as calculated from difference of inflow and outflow samples
212 was considered as nutrient removal. Inflow and outflow concentrations were measured in
213 laboratory from the collected samples.

214 The methane content and volume of the biogas, was measured with GC-FID as described in
215 the literature (Kinnunen et al., 2015). Methane production was converted to normal conditions
216 (NTP): temperature 273 K and pressure 1000 mbar.

217 **3. Results**

218 *3.1. Screening of different dilutions of urine as growth medium*

219 Suitability of undiluted urine (0x), urine with lower dilution ratios (2x - 5x) and higher dilution
220 ratios (10x, 15x, 20x, 25x) as a growth medium for *S. acuminatus* was studied in 7-day batch
221 assays (Fig. 1). The first series of dilutions (0x – 5x) did not support microalgal growth. Slight
222 increase in OD_{660} up to 1 could be observed for 5x dilution on day 4, but the OD_{660} soon reduced
223 below the initial value of 0.8. The second series of dilutions (10x - 15x) showed improvement
224 in microalgal growth for the first 3 days followed by decrease in OD_{660} likely due to cell death
225 after day 4. However, continuous growth was observed in cultures with 20x dilution where
226 OD_{660} constantly increased from 0.9 to 1.4, which was the highest OD_{660} obtained throughout
227 these batch experiments. With 25x dilution there was an initial growth with increase in OD_{660}
228 up to 1.3 after which the OD_{660} decreased to 1.1. In all culture bottles with different dilutions,
229 the starting pH was 8.7 (Fig. 1b) from which the pH continuously increased, while some
230 decrease towards the end of the incubation (after day 4) was seen for the cultures growing on
231 20x and 25x diluted urine.



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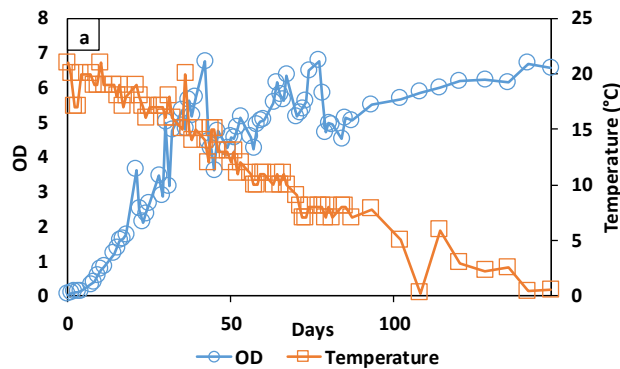
234 **Figure 1:** (a) Growth (as optical density measured at 660 nm) of *S. acuminatus* in human
 235 urine at different dilutions, (b) pH during the batch experiments

236 *3.2. Raceway pond (400 L) operation in batch mode*

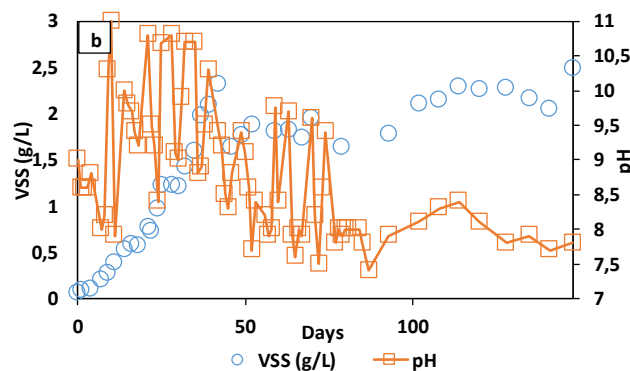
237 *S. acuminatus* was cultivated in batch mode in the SRwP with a working volume of 400 L
 238 containing urine with 20x dilution to study the maximum possible algal growth, measured in
 239 terms of OD₆₆₀ and VSS. Batch growth was conducted for almost five months spreading over
 240 summer (July, days 1-14, temperature 15-20 °C), autumn (August, September and October,
 241 days 15-102, temperature 10-15 °C) and onset of winter (November and December, days 103-
 242 148, temperature < 5 °C). The growth of *S. acuminatus* measured as OD₆₆₀ followed a
 243 continually increasing trend with sudden peaks and drops associated to increase or decrease in
 244 culture solution temperature, respectively (Fig 2a). However, the microalgae recovered and

245 started to grow within a few days after the drops in temperature throughout the entire
 246 experimental period (Fig. 2a). The OD₆₆₀ of the microalgal culture in the pond increased to a
 247 maximum of 6.78 on day 77, and the final OD₆₆₀ value was 6.56 on day 148. Temperature in
 248 the pond was below 10 °C from day 60 onwards, while it was consistently below 5 °C from
 249 day 100 onwards. Around day 148, the outdoor temperature went subzero and the study was
 250 stopped due to freezing of the pond contents.

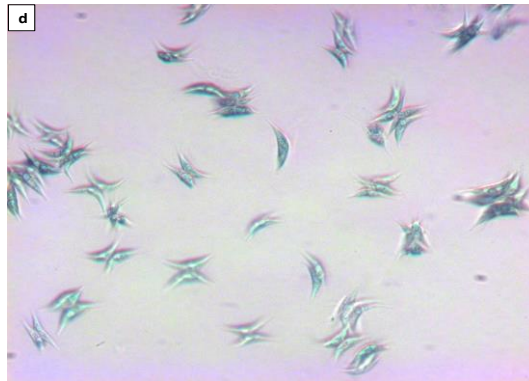
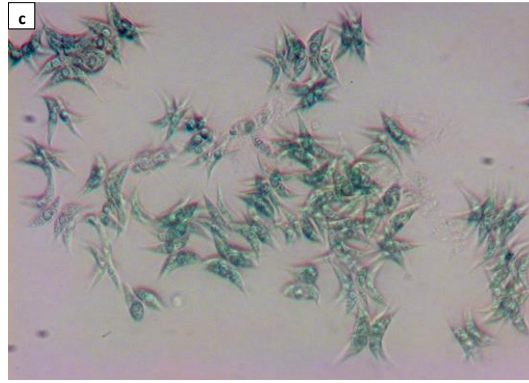
251 VSS in the pond was also monitored to determine if the biomass concentration in g per L
 252 followed similar trend as OD₆₆₀. The maximum VSS of 2.3 g/L (Fig. 2b) was obtained on day
 253 42, when also the maximum OD₆₆₀ was recorded. After day 42, the VSS decreased suddenly
 254 and gradually started to increase again and remained around 2.11 g/L to 2.29 g/L from day 100.
 255 The pH of the ponds fluctuated widely and fast; it varied between 7.4 and 11 for the initial 60
 256 days, after which the variation reduced and pH remained between 7.4 and 8.4 (Fig. 2b).
 257 Microscopic images from day 14 of the experiment (temperature, 19 °C) showed *S. acuminatus*
 258 growing in dense colonies of four cells (Fig. 2c), whereas Fig. 2d shows reduced density of
 259 cells on day 77 when the temperature was 8 °C.



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264 **Figure 2:** Variation of (a) optical density (OD_{660}) and culture temperature, (b) volatile
265 suspended solids (VSS) and pH with time and microscopic image of *S. acuminatus* growing
266 in the small raceway pond on (c) day 14 and (d) day 77

267 3.3. Raceway pond (2000 L) operation in semi-continuous and batch mode

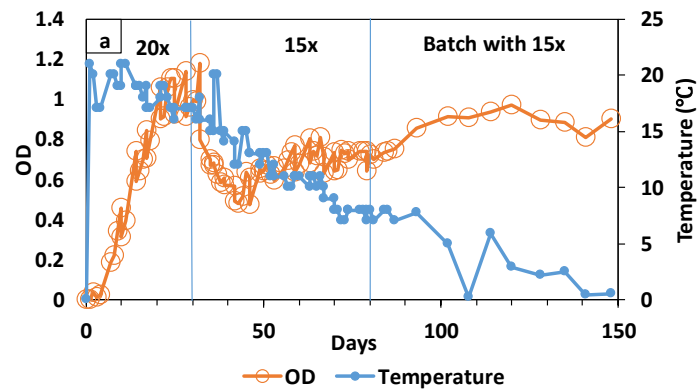
268 *S. acuminatus* was cultivated in a semi-continuously operated raceway pond (BRwP) having a
269 working volume of 2000 L for 148 days. The pond was fed with urine with a dilution of 20x
270 for the first 28 days (from the middle of July to the middle of August, average temperature 17
271 °C). After 28 days, the dilution of urine was reduced to 15x, the semi-continuous feeding of
272 which was continued for 51 days (up to day 79 with a break between days 37 and 45, average
273 temperature 11 °C), after which batch mode operation was continued for 69 days (up to day
274 148, average temperature 7 °C).

275 Higher dilution (20x) supported continuous microalgal growth reaching a maximum OD_{660} and
276 VSS of 1.1 g/L and 0.34 g/L, respectively, after 28 days (Fig. 3). The pH varied widely between
277 8.5 and 11 (Fig. 3). When the urine dilution was reduced to 15x, decrease in microalgal growth
278 was observed with OD_{660} decreasing from 0.99 to 0.68 and VSS from 0.42 g/L to 0.28 g/L in
279 7 days. In addition, the culture turned from healthy green to brownish colour based on visual
280 observations. To recover from the probable shock load, the pond was fed only with tap water

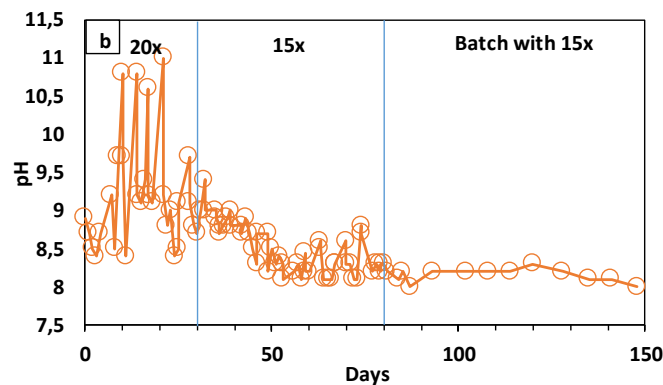
281 for 10 days (days 37 to 45) after which feeding with 15x diluted urine was continued. Between
282 day 49 and 79, the OD₆₆₀ and VSS of the pond culture remained at around 0.70 and 0.31 g/L,
283 respectively. During the batch operation from day 80 onwards, the OD₆₆₀ increased slowly to
284 a maximum of 0.97 on day 120. Though VSS of the pond contents followed a similar trend as
285 that of OD₆₆₀ in general, it did not increase like OD₆₆₀, and was around 0.34 g/L, when the pond
286 was operated in batch mode in the last phase of the experiment. Harvesting efficiency of the
287 microalgal biomass was $57 \pm 8\%$ of VSS with approximately 150 g (75 g per harvesting day)
288 of wet biomass collected every week.

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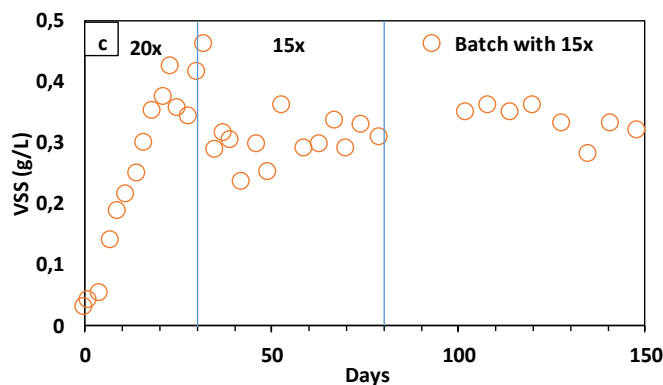
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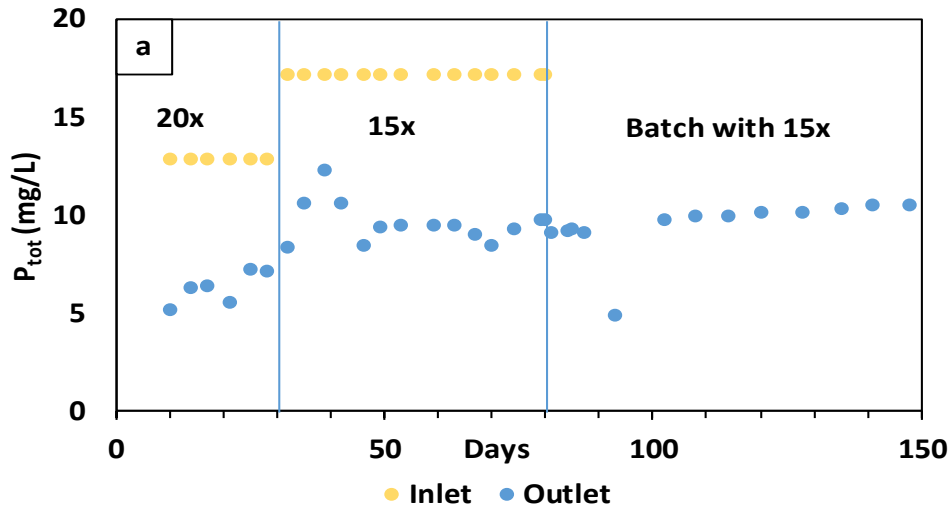
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294 **Figure 3:** Variation of (a) temperature and optical density (OD₆₆₀), (b) pH and (c) volatile
295 suspended solids (VSS) in the large open raceway pond operated with source segregated
296 urine with different dilutions in semi-continuous and batch mode

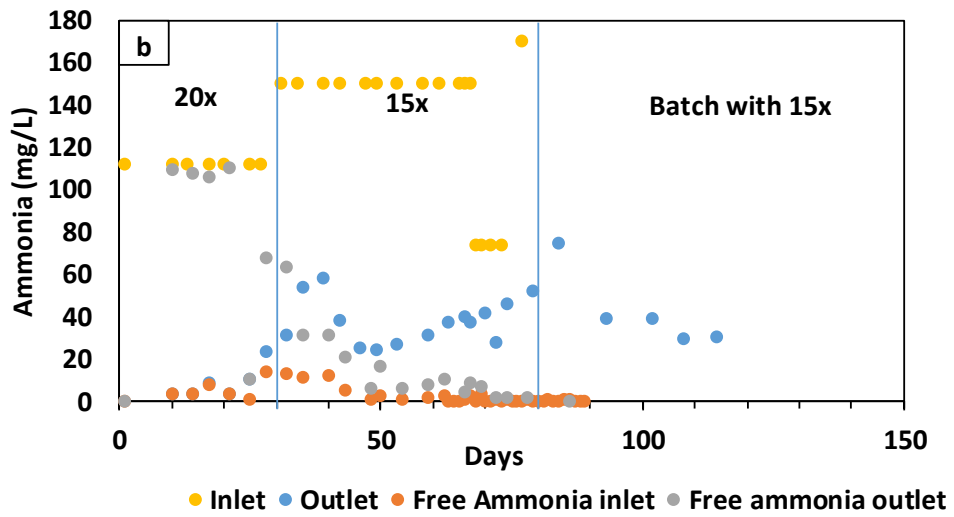
297 The soluble phosphorus, ammonium and soluble TN concentrations in the pond were as shown
298 in Fig. 4. When the pond was operated in semi-continuous mode with 20x diluted urine,
299 removal of approximately 38% of phosphorus, 67% of NH₄⁺ N and 52% of TN in a cycle of
300 15 days was obtained, calculated according to Eq. 2. The removal reduced to around 13%, 18%
301 and 22% for phosphorus, NH₄⁺ N and TN respectively, during semi-continuous operation with
302 15x diluted urine. Almost no removal of the nutrients was observed, while operating the pond

303 in batch mode during the last phase of the experiment. There was no measurable uptake of the
304 trace metals like Na, K, Mg and Ca during the entire period of operation of the pond.

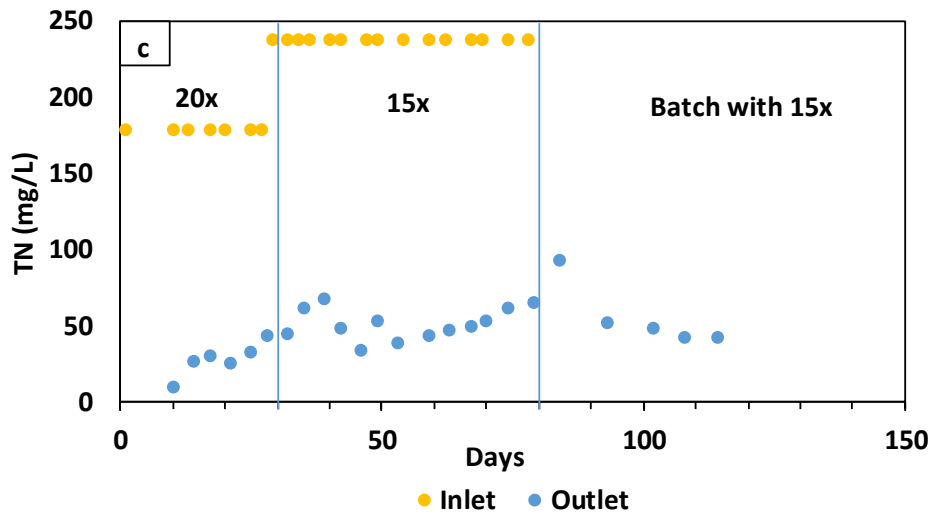
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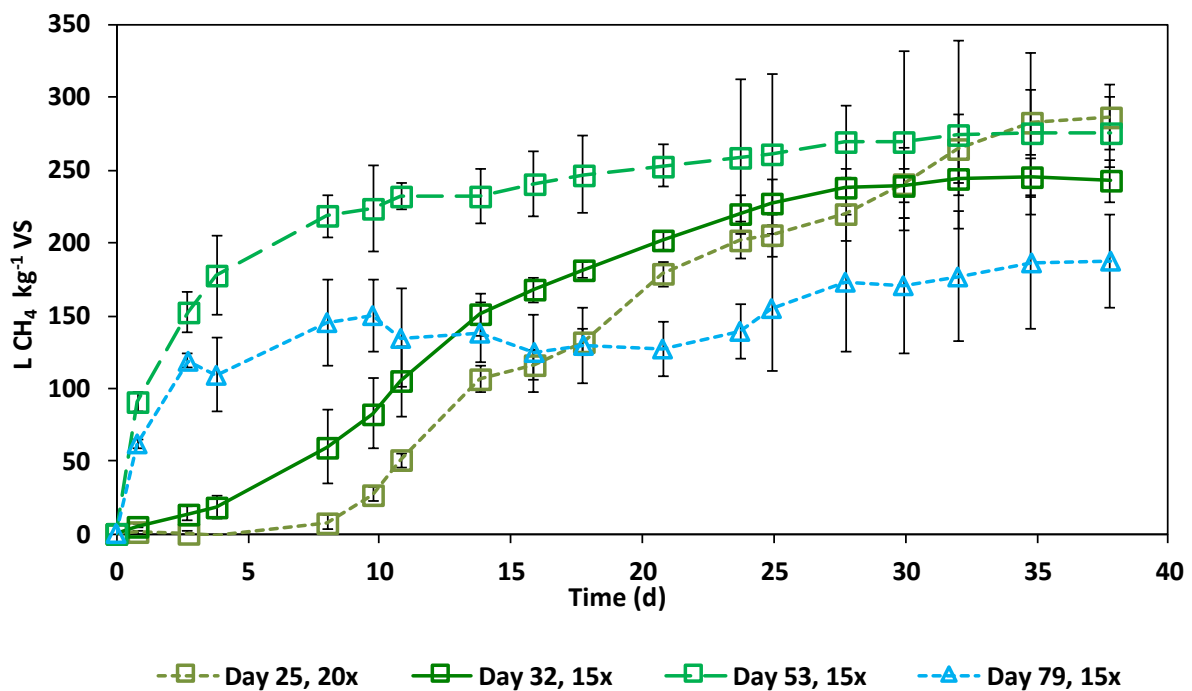


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309 **Figure 4:** Variation of soluble (a) P_{tot} , (b) $NH_4^+ N$, (c) TN in the large open raceway pond
 310 operated with different dilutions in semi-continuous and batch mode

311 3.4. Biomethane generation potential from the harvested microalgal biomass

312 Methane production assays were done on microalgal biomass collected from different phases
313 of growth namely 20x dilution phase (healthy cell growth, day 25, freeze dried), 15x dilution
314 start phase (cells were dying, day 32, freeze dried), and 15x dilution stable phase (freeze dried,
315 day 53 and stored as such day 79) (Fig. 5). Methane production started immediately for two of
316 the biomass samples, collected on 15x growth phase (freeze dried, day 53 and as such stored,
317 day 79), and 70–90% of the total methane was formed within 10 days from the beginning of
318 the assay. The initial methane production rate for the biomass samples collected on day 25 (20x
319 dilution) and day 32 (15x dilution) was slower than the other two samples (Fig. 5). While the
320 biochemical methane potential (BMP) of the harvested biomass (day 53, 15x and day 25, 20x)
321 after freeze-drying was above 250 L/kg VS, it was less than 200 L/kg VS for the biomass
322 without freeze-drying. For the freeze-dried biomass, maximum BMP was found during
323 cultivation with 20x urine (285 ± 20 L/kg VS) followed by that harvested during growth phase
324 with 15x dilution (275 ± 25 L/kg VS) and the lowest BMP (250 ± 15 L/kg VS) was observed
325 for the time period when the algal cells were dying, during change in urine dilution (day 32).



326

327 **Figure 5:** Cumulative methane production from the harvested microalgal biomass samples
328 taken on different days of cultivation

329

330 4. Discussion

331 4.1. Screening urine dilutions for culturing of *S. acuminatus* in laboratory conditions

332 *S. acuminatus* was chosen for this study because of its extensive use in wastewater treatment
333 research for, e.g. in anaerobic digestion effluents (Tao et al., 2017b) and secondary domestic
334 wastewater (Posadas et al., 2015), and because of its capacity to grow in high biomass
335 concentrations of 8 – 11 g/L (Tao et al., 2017a,b). Treatment and nutrient recovery from human
336 urine with microalgae would be most advantageous when the urine is used without dilution.
337 Therefore, the main objective of the dilution screening experiments was to find out the lowest
338 possible dilution of urine in which microalgae can effectively grow. The results showed that in
339 batch experiments *Scenedesmus* could grow at 10x dilutions (initially 200 mg/L of ammonia-
340 N) and not at lower dilutions, but proper growth without significant decrease in biomass
341 concentration after initial growth could only be observed at 20x dilution (initially 100 mg/L of
342 ammonia-N).

343 Human urine is a very concentrated nutrient solution. Among the nitrogen compounds urea is
344 dominating in fresh urine, but when urine is stored, urea hydrolyzes to ammonia and carbon
345 dioxide (Adamsson, 2000). Microalgae can assimilate ammonium directly into organic
346 compounds, which could explain the rapid initial algal growth in the diluted urine. Unionized
347 or free ammonia, which increases with increasing pH, could be toxic for algae, depending on
348 the species, at a concentration around 50 mg/L (Azov and Goldman, 1982; Udert et al., 2006).
349 High pH levels (pH > 10) in this study, caused by the buffering capacity of carbonate and
350 ammonia and also due to uptake of HCO_3^- ions during algal photosynthesis, can also lead to
351 precipitation of unchelated iron, phosphate and carbonate, which then become unavailable for
352 microalgal uptake (Kawasaki et al., 1982; Udert et al., 2006). The decreased pH at the end of
353 incubation period was apparently due to ammonium uptake by algae, which results in H^+
354 production lowering pH. High pH can also indicate that the cultures were likely CO_2 limited
355 and the decrease in pH in the end indicates reduced growth.

356 Also some previous studies have reported limited or no growth of microalgae on dilutions of
357 urine lower than 20x in batch experiments. For example, limited growth of *Arthospira*
358 *platensis*, with OD_{660} below 0.2, was reported by Coppens et al. (2016) in hydrolyzed human
359 urine at 5000 times dilution. When *Chlorella sorokiniana* was cultivated in 5x diluted
360 hydrolysed urine, OD_{750} increased from 0.1 to approximately 0.3 in one day but from the
361 second day onward OD_{750} did not show any increase (Tuantet et al., 2014). The same

362 phenomenon was observed in urine without any dilution. Tuantet et al. (2014) also tested 20x
363 dilutions and concluded that 20x dilution showed the highest growth, as the OD₇₅₀ rose from
364 0.1 to 0.8 in one day without addition of trace elements.

365 Growth of microalgae like *Spirulina* on much higher dilutions of fresh human urine (120 times)
366 has been reported by Chang et al. (2013). However, the fresh human urine studied by Chang et
367 al. (2013) had higher concentrations of N_{tot} (8800 mg/L) and P_{tot} (792 mg/L) than the source
368 separated stored urine used in this study (N_{tot}: 3480 ± 130 mg/L, P_{tot}: 190 ± 52 mg/L).
369 Microalgal growth (*Chlorella vulgaris*) was reported to follow similar growth rates for all urine
370 dilutions (1:25 to 1:100), with somewhat higher growth at a dilution of 1:100 (0.6 g/L VSS)
371 compared to that at 1:25 dilution (0.52 g/L VSS) and 1:300 dilution (0.48 g/L VSS) (Jaatinen
372 et al., 2016). Growth of microalgae on human urine depends a lot on the pH, temperature, light
373 intensity and reactor configuration, as these parameters determine the availability of
374 phosphorus, nitrogen and trace elements, and at the same time toxicity of nitrogen. Hence, it is
375 difficult to conclude from laboratory studies conducted in controlled environment as to what
376 would happen in real-life conditions, such as raceway ponds, necessitating pilot-scale studies.

377 4.2. Cultivation of *S. acuminatus* in the raceway ponds

378 The maximum OD₆₆₀ of 6.8 obtained in the batch raceway pond of volume 400 L fed with 20x
379 diluted urine after 40 days of cultivation was comparable to growth in the synthetic modified
380 N8 medium, where the maximum OD₆₆₀ was 6.4 in 8 days. The maximum OD obtained in the
381 small raceway pond was much higher than the maximum OD₆₆₀ of 1.3 as obtained on 4th day
382 of cultivation in the batch bottles containing the same dilution of urine. The average light
383 irradiation, ambient temperature, number of daily sun hours and evaporation rates decreased
384 throughout the operational period of the pond. With the decreasing temperature (below 15 °C)
385 and shorter days with decreasing light intensities, the microalgal growth decreased (OD₆₆₀ <
386 4.5) from day 43 onwards. However, the growth rate started to steadily increase after a slow
387 growth and also probable cell death for around 20 days and OD₆₆₀ reached the value of 6.8
388 again on day 77 when the average temperature was just 10 °C for the last 20 days. Although
389 optimum temperatures for microalgal growth often range from 20 to 30 °C, successful carbon
390 and nutrient removal from piggery (Godos et al., 2009) and municipal wastewaters (Posadas et
391 al., 2015) has been reported in raceway ponds, of respective volumes 464 L and 800 L, at
392 average mixed liquor temperatures of 7 to 11 °C.

393 Increasing pH might lead to ammonia toxicity, due to increase in free ammonia concentration
394 (Adamsson, 2000), which however, is not so pronounced at lower temperatures (Udert et al.,
395 2006). In this study ammonia N concentration in the 15x and 20x diluted urine was around 120
396 and 90 mg NH₄-N/L, respectively, which should not be toxic to *S. acuminatus* (Tao et al.,
397 2017a). For example, Tao et al. (2017a) observed growth of *Scenedesmus* in laboratory scale
398 photobioreactors even at ammonia concentrations as high as 480 NH₄-N/L. Thus, hindered
399 growth in the ponds were likely due to low temperature and shorter daylight period. However,
400 these variations are unavoidable in the Nordic outdoor conditions.

401 A semi-continuous cylindrical reactor was operated by Adamsson, (2000) on 50x diluted
402 human urine for the growth of *S. acuminatus* and a maximum biomass concentration of 287
403 mg/L (VSS) was reported after supplementing with iron, magnesium and EDTA. In this study,
404 a higher biomass concentration of 424 mg VSS/L at 20x dilution and 460 mg VSS/L at 15x
405 dilution indicates higher availability of nutrients at lower dilutions. Tuantet et al., (2014b) also
406 observed increased growth of *Chlorella sorokiniana* in synthetic human urine in a 1 L
407 photobioreactor with 5 times diluted synthetic urine and a light intensity of 490 mmol
408 photons/m².s (6 g VSS/L) as compared to 20 times dilution and 990 mmol photons/m².s (2.9 g
409 VSS/L), probably due to more availability of nutrients.

410 The current study is the first reporting microalgal growth in source separated human urine in
411 open raceway ponds in Nordic climate. Growth of algae at low temperatures, lower light
412 irradiance and shorter daylight time indicates potential of use of microalgal ponds to treat urine
413 in Nordic areas. However, more detailed evaluation to understand the limiting factors and
414 ultimately optimize the pond performance is necessary.

415 *4.3. Removal of nitrogen and phosphorus*

416 When the big pond was operated in semi-continuous mode with 20x diluted urine, removal of
417 around 38% of soluble phosphorus, 67% of NH₄⁺-N and 52% of TN was observed. The TN
418 removal efficiency was higher, while phosphorus removal was lower to the ones reported by
419 Adamsson (2000), (23% removal of TN, 57% removal of soluble phosphorus) while cultivating
420 *Scenedesmus* in a pilot-scale (40 L) cylindrical photobioreactor on 50x diluted urine. However,
421 the nutrient removal in the current study is a combination of phosphate precipitation, ammonia
422 loss to environment due to volatilization and microalgal uptake. García et al. (2000)
423 demonstrated that the loss of ammonia to the atmosphere was the most important mechanism
424 for nitrogen removal in algal ponds, the percentage of which increases with increasing pH. The

425 presence of un-ionized ammonia increases as pH rises leading to stripping off ammonia and
426 vice versa ($\text{NH}_3 + \text{H}^+ \leftrightarrow \text{NH}_4^+$). In this study, the pH of the microalgal cultures fluctuated
427 between 7.5 and 11 in the small pond and between 8 and 11 in the big pond. Higher pH would
428 lead to higher loss of ammonia to the atmosphere (Chang et al., 2013). Change in temperature
429 makes ammonia to solubilize or volatilize (increasing free ammonia concentration with
430 increasing temperature), causing changes in pH. Fluctuations in pH reduced slowly with
431 decreasing temperature during this study (after day 50, average temperature $< 10^\circ\text{C}$)
432 decreasing the changes in ammonia volatilization. Future studies with continuous monitoring
433 of pH or even pH control, temperature and ammonia concentration in different forms would
434 give more understanding on the fate of nutrients. Again, this loss through ammonia evaporation
435 may be the most important mechanism for N removal in this study, but this assumption requires
436 further studies.

437 The concentration of soluble P_{tot} decreased for the first seven days of the semi-continuous
438 operation from 6.31 mg/L to 3.26 mg/L for 20x diluted urine and from 10.10 mg/L to 7.56
439 mg/L for 15x diluted urine. After seven days the concentration remained either constant or was
440 observed to increase at some point, indicating a break in phosphate uptake by algal cells.
441 Jaatinen et al. (2016) reported, with 1:25-diluted urine in batch cultivation, a final P_{tot}
442 concentration of 9.4 mg/L (from initial 14 mg/L) in 10 days, after which the concentration
443 remained unchanged. Alkaline pH leads to the transformation of H_2PO_4^- present in urine into
444 HPO_4^{2-} and PO_4^{3-} , which can precipitate with Ca^{2+} and Mg^{2+} in urine (Chang et al. 2013). With
445 changing pH, there could be precipitation and dissolution of the phosphate (Chang et al., 2013).
446 This could be the reason why in this study an increase in phosphate concentration was
447 occasionally observed during the operation of the big pond (for example during days 35 to 49).
448 In addition, dying algal cells can release the phosphorus and nitrogen from the cells thus
449 increasing the phosphate in the medium (Jaatinen et al., 2016). Thus, it is difficult to quantify
450 exact amount of phosphate uptake and detailed speciation study is required for that.

451 Bryant and Appah (2017) observed that *Scenedesmus* removes more phosphorus than nitrogen
452 from diluted human urine and that removal of phosphorus increases with decreased molar ratio
453 of nitrogen and phosphorus and also, with decreasing light intensity. The results obtained in
454 the current study was in contrast with that reported by Bryant and Appah (2017). However, the
455 experiments by Bryant and Appah (2017) were conducted under controlled laboratory
456 conditions in 250 mL flasks and in this study various parameters changed simultaneously. A
457 study by Posadas et al. (2015), also revealed lower phosphate removal (57%) than nitrogen

458 removal (79%). Hence, it is obvious that there are other factors, or probably interaction of
459 several factors that can change the nutrient uptake proportions in large scale outdoor cultivation
460 of microalgae.

461 4.4. Methane production from harvested algal biomass

462 One of the challenges in this study was the harvesting of microalgal biomass using simple
463 filtration. Only approximately 50% of the microalgal biomass growing in the pond could be
464 harvested with the filter cloth. Nevertheless, screening for efficient harvesting method was not
465 the main objective of this research and future studies employing efficient and continuous
466 harvesting is necessary.

467 Varying BMPs between 107 and 410 L CH₄ kg⁻¹ VS have been found for *Scenedesmus*
468 dominating biomass, mainly cultivated in different synthetic media (Frigon et al., 2013;
469 Kinnunen and Rintala, 2016; Roberts et al., 2016; Zhen et al., 2016). Roberts et al. (2016)
470 reported that the BMP of laboratory culture of *Scenedesmus* grown in artificial Jaworski's
471 medium had a much higher BMP (261 L CH₄ kg⁻¹ VS) as compared to that grown in a
472 bioreactor with synthetic fertilizers (161 L CH₄ kg⁻¹ VS) probably due to more challenging
473 growth conditions in the large-scale bioreactor. The BMP of urine grown microalgal biomass
474 in the present study (250 – 300 L kg⁻¹ VS) is comparable to the earlier reported values in
475 synthetic media. The differences in the methane production of algal cells harvested on different
476 days of cultivation could be explained by the different cell composition due to the difference
477 in growth conditions (Kinnunen and Rintala, 2016) like light intensity, temperature and pH.
478 The different growth conditions lead to different uptake of nutrients and likely a varying cell
479 composition. The current study was not designed to realize the impact of different parameters
480 on BMP, hence, further research is needed to understand the difference of BMP depending on
481 growth conditions and health of algal cells. The results and previous reported BMP values
482 clearly indicate that a much deeper knowledge of the factors affecting the anaerobic
483 biodegradability of microalgal biomass is desirable for understanding the heterogeneity of this
484 material as a potential renewable energy source via anaerobic digestion. However, this study
485 was sufficient to state the feasibility of using the algal cells grown on human urine for methane
486 production. Also, it could be noted here that there was a large difference between freeze-dried
487 biomass and the biomass stored as such. The freeze-drying likely acted as a pretreatment step
488 by breaking some of the microalgal cell. However, this kind of pretreatment would not be

489 feasible at larger scale and possibility to avoid freeze drying yet maintaining the same BMP
490 should be explored.

491 *4.5.Extrapolations towards scale up*

492 This study showed that microalgal cultivation is feasible in open raceway ponds on diluted
493 human urine without any additional trace elements or CO₂ supplementation. City of Tampere
494 expects around 20,000 people to start living in the old industrial area of Hiedanranta. While
495 daily production of urine for around 20,000 people would be somewhere around 30 m³/d,
496 volume of urine to be stored for six months would be just around 5400 m³. Based on the present
497 results, 6000 m³ microalgal pond with a surface area of around 2 ha would be needed to treat
498 the urine produced from 20,000 people, when the pond is operated at an HRT of 15 d and a
499 dilution of 15x. Final TP and TN concentrations in the pond, as achieved in this study, were
500 around 7 mg/L and 30 mg/L, respectively. Thereby some form of post treatment is required
501 before discharge. At this stage, use of such huge land area appears unrealistic to realize in
502 practice. Thus, there is a need to reduce the HRT and urine dilution in order to reduce the land
503 area requirement. It might also be interesting to try new reactor designs that would lead to more
504 compact reactor structures and increased nutrient recovery. Research efforts are needed on
505 efficient and automated biomass harvesting and other downstream processing of the harvested
506 biomass. Nevertheless, based on the results of this study, microalgal pond can remove around
507 55 kg/d of TN and 2.3 kg/d of TP, when scaled up for 20,000 people. The algal biomass grown
508 on urine of the entire population of the district could be used to produce around 33,000 m³ of
509 methane per year (Table 2).

510

511 Table 2: Extrapolation of the methane production potential from microalgal biomass grown in
 512 diluted human urine for nutrient recovery in a district with 20,000 inhabitants

TN removed	55 kg/d
TP removed	2.3 kg/d
Maximum VS	0.74 g/L
Methane production	275 L/kg VS
For an HRT of 15 d, methane production	27 L/d or 10,000 L/year
At 15x dilution, urine required	133 L or 9 L/d for an HRT of 15 d

513

514 **Conclusions**

515 This study showed that diluted source separated human urine could provide enough nutrients
 516 to support microalgal growth in open raceway ponds. The study also revealed that it is possible
 517 to grow microalgae even at cultivation temperatures as low as 1 °C. *S. acuminatus* was grown
 518 on diluted urine in raceway ponds without addition of trace elements, artificial light or CO₂.
 519 However, in these conditions and in simple open pond systems, the urine has to be 20-times
 520 diluted to enable reasonable growth. The growth of microalgae in urine was comparable to its
 521 growth in synthetic media in laboratory reactors. *S. acuminatus* removed around 1500 kg/kg
 522 VS.d of TN, 50 kg/kg VS.d of TP from the urine and the produced biomass had a maximum
 523 methane production potential of 285 L CH₄/kg VS. Future studies are planned using more
 524 efficient harvesting methods, focusing on the nutrient mass balance.

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