

1 **Monitoring quantitative dynamics of *Thermotoga neapolitana* in synthetic**
2 **co-cultures using quantitative real-time PCR**

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10 **ABSTRACT**

11 This study demonstrates the potential for biohydrogen production in a co-culture
12 of two ecologically distant species, *T. neapolitana* and *C. saccharolyticus*, and the
13 development of a quantitative real-time PCR (qPCR) method for quantifying the
14 hyperthermophilic bacterium of the genus *Thermotoga*. Substrate utilization and H₂
15 production performance was compared to those of their individual cultures. The highest
16 H₂ yields obtained were 2.7 (±0.05), 2.5 (±0.07) and 2.8 (± 0.09) mol H₂/mol of glucose
17 for *C. saccharolyticus*, *T. neapolitana* and the co-culture, respectively. Statistical
18 analysis comparing the H₂ production rate of the co-culture to either *C. saccharolyticus*
19 or *T. neapolitana* pure cultures indicated a significant difference in the H₂ production
20 rate (p<0.05: t-test), with the maximal rate of H₂ production (36.02 mL L⁻¹ h⁻¹) observed
21 from the co-culture fermentations. In order to monitor the presence of *T. neapolitana* in
22 the bioprocess, we developed a qPCR method using 16S rDNA and hydrogenase
23 (*hydA*) gene targets. The qPCR data using *hydA* primers specific to *T. neapolitana*

24 showed an increase in *hydA* gene copies from 3.32×10^7 to 4.4×10^8 *hydA* gene copies
25 per mL confirming the influence of *T. neapolitana* in the synthetic consortium.

26

27 *Key words:* *Thermotoga neapolitana*; *hydA*; 16S rDNA gene; Real-time
28 quantitative polymerase chain reaction; Hydrogen production; Primer design.

29

30 **1. INTRODUCTION**

31 The global trends of fossil fuel depletion and impact on climate change due to
32 over exploitation of natural resources has led to a search for alternative measures to
33 produce renewable energy [1,2]. Today, hydrogen (H_2) is used in the chemical industry
34 as a fundamental building block e.g. for the production of ammonia-fertilizers and
35 methanol used for manufacturing of many polymers [3]. Hydrogen is presently produced
36 from natural gas, heavy oils, naphtha and coal [4,5] which are not sustainable
37 feedstocks. Hence, there is a need for alternative hydrogen production routes. One of
38 the means that have been highly considered for sustainable energy is biological
39 hydrogen production [6–9].

40 Research on biological H_2 production has increased over the years leading to
41 several reports on methods such as: direct and indirect photolysis, water-gas shift
42 reaction, photofermentation, biocatalysed electrolysis and dark fermentation [10,11].
43 Dark fermentation has garnered interest due to the ability to utilize a wide variety of
44 waste streams and energy crops as substrate for hydrogen production, and high
45 hydrogen production rates ($10\text{--}15 \times 10^3$ ml H_2 /l/h) [7,12]. Dark fermentative H_2

46 production can occur under mesophilic (typically between 30-45 °C), thermophilic (50-
47 60 °C) or hyperthermophilic conditions (from 60 °C upwards). Compared to mesophilic
48 conditions, higher temperatures favor H₂ production [13,14], because the temperature at
49 which the reaction takes place affects the thermodynamic process according to $\Delta G^0 =$
50 $\Delta H - T\Delta S^0$ and increases the kinetics of chemical reactions thereby speeding up the
51 reactions [15,16].

52 Several bacterial species have been identified for their ability to produce high
53 volumes of H₂ at hyperthermophilic conditions. An example is the bacterium
54 *Thermotoga neapolitana*. In recent years, there has been a significant increase in the
55 studies on *T. neapolitana*, as it has enabled one of the best H₂ yields (3.8 mol H₂/mol
56 glucose) that have been reported in literature [20, 21]. Combined with its ability to
57 produce high H₂ yields at elevated temperatures (55 - 85 °C), *T. neapolitana*, is capable
58 of metabolizing a wide range of simple and complex carbohydrates such as hexoses,
59 pentoses, disaccharides, glucan and amorphous cellulose [24–27]. Previous studies on
60 *T. neapolitana* have focused in optimizing growth and H₂ production conditions for pure
61 cultures of members of *Thermotoga* sp. [18,19]. However, molecular methods are still
62 needed to better understand and answer questions relating to *T. neapolitana*'s
63 physiological, ecological and metabolic features. A deeper understanding of the
64 bacterium will allow for its metabolic engineering and use in biotechnological
65 applications. Developing molecular methods for monitoring the activity of *T. neapolitana*
66 in various systems require a more accurate representation that would take into account
67 their dynamics and interactions in a mixed consortium while carrying out individual
68 metabolic processes.

69 Reports on biohydrogen production from hyperthermophilic microorganisms have
70 mostly utilized conventional methods for monitoring the growth of the microbial
71 population such as dry cell weight, optical density (biased in the case of floc formers like
72 *T. neapolitana*) or microscopy [17–23]. Some of these methods are only suitable for
73 monocultures and fail to differentiate between different species. Furthermore, members
74 of the genus *Thermotoga* undergo floc formation which often causes ambiguities in cell
75 enumeration [28].

76 In the present work, co-cultivation of two ecologically distant organisms for
77 improved H₂ evolution and the development of a quantitative PCR assay for genus and
78 species-level monitoring of *Thermotoga* was carried out. The 16S rDNA method was
79 designed to target eight members of the group *Thermotoga*. Given the high degree of
80 similarity and absence of correlation that may occur between 16S rDNA and H₂
81 producing activity in *T. neapolitana*, we further developed a qPCR approach targeting
82 the hydrogenase A (*hydA*) gene for a more comprehensive evaluation of *T. neapolitana*
83 in a synthetic culture. To our knowledge, studies targeting the hydrogenase gene for
84 specie-level monitoring of hyperthermophiles have not been previously published.

85 **2. MATERIALS AND METHODS**

86 **2.1. Bacterial strains and growth conditions**

87 Bacterial strains *Thermotoga neapolitana* DSM-4359, *Thermotoga maritima* DSM-3109
88 and *Caldicellulosiruptor saccharolyticus* DSM-8903 (DSMZ, Germany) were used in this
89 study. *T. neapolitana* was cultivated either as a pure culture or with *C. saccharolyticus*
90 as a synthetic co-culture. The medium used for cultivation of *T. neapolitana* contained

91 the following components (g/L): NH₄Cl, 1.0; K₂HPO₄, 0.3; KH₂PO₄, 0.3; MgCl₂ x 6 H₂O,
92 0.2; CaCl₂ x 2H₂O, 0.1; NaCl, 5.0; KCl, 0.1; cysteine-HCl, 1.0; yeast extract, 2.0; 10.0 ml
93 L⁻¹ of vitamin and trace element (DSMZ 141, Germany) solution. *C. saccharolyticus*
94 pure culture was initially maintained in DSMZ 641 medium. The initial medium pH was
95 adjusted to 7.5 (20 °C) for all cultures with 5 M NaOH. Thirty milliliter of the prepared
96 media was dispensed anaerobically into 120 ml serum bottles. The bottles were sealed
97 with butyl rubber stoppers, capped with aluminum crimps and autoclaved for 15 min at
98 121 °C. Unless otherwise mentioned, glucose (20mM) was added after sterilization and
99 the bottles containing the growth medium were inoculated with 10 % (v/v) inoculum
100 under anoxic conditions. Triplicate cultivations of *T. neapolitana* and *C. saccharolyticus*
101 as a pure culture and as a synthetic co-culture were carried out. Cultures were
102 incubated at 75°C and 150 rpm for 1-100 hours. To validate the specificity of the
103 primers developed in this study, microbial community from a H₂ producing fluidized bed
104 bioreactor without *Thermotoga* was used [29] as well as pure cultures of *T. neapolitana*
105 and *C. saccharolyticus*.

106 **2.2. Analytical techniques**

107 The cell concentration of the culture suspension containing bacterial cells was
108 determined by measuring the absorbance spectrometrically with an Ultraspec 200 Pro
109 spectrophotometer (Amersham Biosciences, Munich, Germany) at 600 nm. Hydrogen
110 and carbon dioxide levels in the gas phase were measured at regular intervals to
111 monitor the activity of the microbial consortium. The total gas volume was first
112 measured by releasing the pressure in the culture using a syringe [30]. The headspace
113 of each culture bottle was sampled using a gas tight syringe with 0.2 mL injection

114 volume. The gas composition was then analyzed with a Shimadzu gas chromatograph
115 GC-2014 equipped with a Porapak N column (80/100 mesh) and a thermal conductivity
116 detector. Nitrogen was used as the carrier gas and the injector, column and detector
117 temperatures were 110 °C, 80 °C and 110 °C respectively. The total volume of the gas
118 produced at each time point was calculated using equation 1 [29,31]:

$$119 \quad V_{H_2,t} = V_{H_2,t-1} + C_{H_2,t}(V_{G,t} - V_{G,t-1}) + V_H(C_{H_2,t} - C_{H_2,t-1}) \quad (1)$$

120 Where $V_{H_2,t}$ is the cumulative hydrogen gas produced at time t, $V_{H_2,t-1}$ is the cumulative
121 hydrogen gas produced at time t-1, $V_{G,t}$ is the total gas volume at time t, $V_{G,t-1}$ is the
122 total gas volume at time t-1, $C_{H_2,t}$ is the hydrogen gas fraction in the headspace at time t,
123 $C_{H_2,t-1}$ is the hydrogen gas fraction in the headspace at time t-1 and V_H is the total
124 headspace volume in the culture bottle. Glucose, lactate and acetate and ethanol were
125 measured using a high performance liquid chromatograph (HPLC) equipped with a
126 Rezex RHM-monosaccharide H+ (8%) column (Phenomenex, USA) and a refractive
127 index detector (Shimadzu, Kyoto, Japan). The mobile phase used was 0.01 N H₂SO₄ at
128 a flow rate of 0.6 mL/min. At the end of 100 h period of incubation, samples from the co-
129 cultures were harvested, centrifuged and stored at -20 °C for genomic isolation and
130 molecular analyses.

131 **2.3. Genomic DNA isolation**

132 Genomic DNA of both pure (*T. neapolitana*, *T. maritima* and *C. saccharolyticus*)
133 and synthetic co-cultures of *T. neapolitana* and *C. saccharolyticus* were isolated with
134 Blood and tissue genomic DNA extraction miniprep system (Viogen, USA) according to

135 the manufacturer's instructions. The protocol was optimized by including three freeze
136 and thaw cycles to enhance genomic DNA recovery.

137 **2.4. 16S rDNA and *hydA* primer design**

138 In this study 16s rDNA and *hydA* were targeted for genus and species level
139 monitoring of *Thermotoga* sp. The 16S rDNA primers for the members of *Thermotoga*
140 sp. was designed with Clustal Omega software
141 (<http://www.ebi.ac.uk/Tools/msa/clustalo/>). The multiple sequence alignments were
142 designed to contain four different bacterial species from three genera: *T. neapolitana*, *T.*
143 *maritima*, *C. saccharolyticus*, *Thermoanaerobacterium thermosaccharolyticum*. The
144 region, conserved only for *Thermotoga* sp. were selected and employed in the primer
145 designing using the Primer-BLAST (<https://www.ncbi.nlm.nih.gov/tools/primer-blast/>).
146 Primer specificities towards 16S rDNA of *Thermotoga* sp. were evaluated using arb-
147 silva (<https://www.arb-silva.de/search/testprime/>), an *in silico* PCR analysis tool which
148 uses 16S/18S rDNA non-redundant reference dataset, SSURef 108 NR [32].

149 The primers were designed to have an amplicon length of 100 to 150 bp and
150 primer melting temperature of 55 °C to 60 °C. The G+C content was between 50 - 60%
151 with not more than three consecutive G or C bases in the primer sequence. The
152 specificity of the primers was manually verified using nucleotide BLAST. Based on the
153 nucleotide sequences, a primer set was designed to amplify the 16S rDNA gene of
154 *Thermotoga* sp. (Fwd, 5'-TACCCCATACGCTCCATCAA-3'; Rev, 5'-
155 CCGTTACCCACCAACTAC-3') and *T. neapolitana hydA*
156 (*hydA*_F_AGTACACGGCATGAAGGAGA; *hydA*_R_CGCAGAACACA ACTATCCAC-3').
157 The applicability and specificity of the developed primers was tested using the hydrogen

158 producing cultures of *T. neapolitana*, *T. maritima*, *C. saccharolyticus* and mixed cultures
159 from fluidized bed bioreactor, known to contain members of the genus
160 *Thermoanaerobacterium* [29]. Melt curve analysis was conducted simultaneously with
161 the real-time quantitative PCR (qPCR) and the success of the assays (qPCR products)
162 was evaluated on agarose gel electrophoresis (1 % agarose, 0.2 V for 20 min).

163 **2.5. Real-time quantitative PCR**

164 Optimization of primer annealing temperatures for 16S rDNA and *hydA* genes
165 were performed by testing six annealing temperatures for 16S rDNA and *hydA*
166 amplifications (48 °C, 53 °C, 55 °C, 58 °C, 60 °C and 65 °C) separately for both primer
167 pairs. *T. neapolitana* genomic DNA was used as the template to generate the standard
168 curve and the assays were conducted using 10-fold serial dilutions of the template DNA.
169 Genomic standards were subsequently run simultaneously with unknown samples to
170 determine the gene copy number (gene copies per mL) and the copy number of *T.*
171 *neapolitana* was calculated based on the genome size (1.88 Mb). The amplifications
172 were carried out in triplicates with the Applied biosystems StepOnePlus real-time PCR
173 (ThermoFisher Scientific, USA). Each 20 µL qPCR reaction mixture contained 10 µL of
174 Maxima SybrGreen/ROX qPCR master mix (Thermo Scientific, USA), 0.4 µL each of 10
175 µM forward and reverse primers, 7.2 µL of nuclease free water and 2 µL of genomic
176 DNA as template. The qPCR conditions were as follows: 10 min at 95 °C followed by an
177 extension step of 40 cycles of 15s at 95 °C and 1 min at 60 °C. To determine primer
178 specificity, melt curve analysis was done under the following conditions: 15 s at 95 °C, 1
179 min at 65 °C and 15 s at 95 °C. The slope and y-intercept of the standard curves were
180 evaluated using a linear regression analysis [33]. Gene copies per ng of DNA extracted

181 and the gene copies per sample were evaluated according to equation 2 and 3,
182 respectively [34]. The amplification efficiencies were calculated using equation 4.

183

$$184 \text{ Gene copies} = \text{DNA}_{[\text{ng}/\mu\text{L}]} \times \frac{1\text{g}}{1000^3\text{ng}} \times \frac{1\text{ mol bp DNA}}{660\text{ g DNA}} \times \frac{6.023 \times 10^{23}\text{bp}}{\text{mol bp}} \times \frac{1\text{ copy}}{\text{genome size}_{\text{bp}}} \times \text{vol. DNA used}_{\mu\text{L}} \quad (2)$$

185

$$186 \text{ Gene copies per sample volume} = \frac{(\text{gene copies per rxn mix}) \times (\text{volume of DNA in } \mu\text{L})}{(\text{volume of DNA template per rxn mix}) \times (\text{volume of sample used})} \quad (3)$$

187

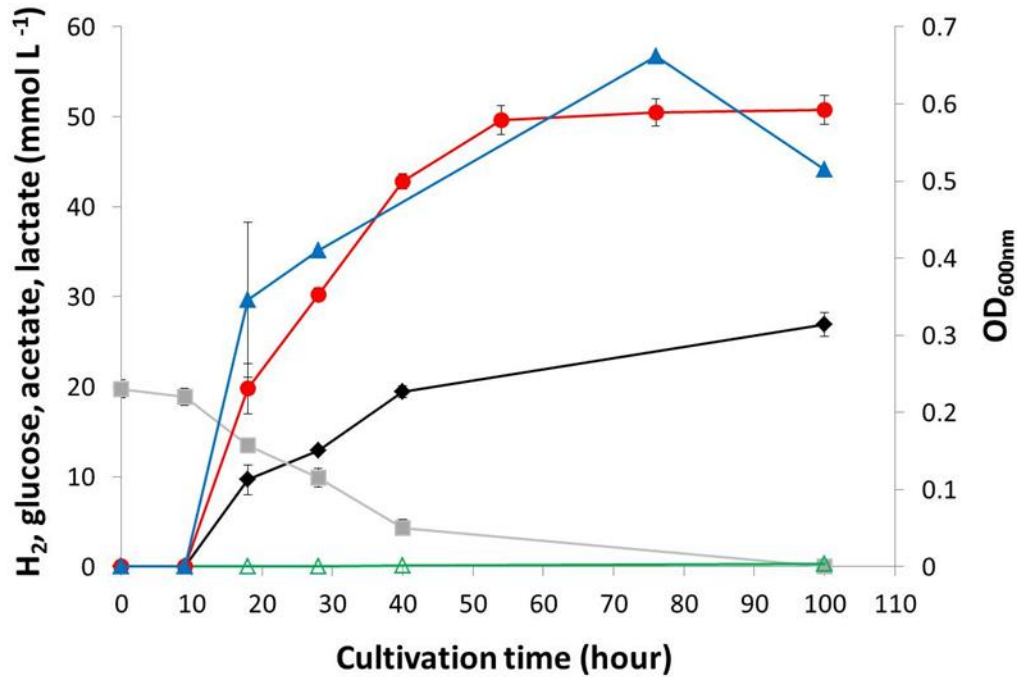
$$188 \text{ Efficiency} = [-1 + 10^{(-\frac{1}{\text{slope}})}] \quad (4)$$

189 3. RESULTS AND DISCUSSION

190 3.1. Comparing hydrogen production between individual cultures and co- 191 cultures of *T. neapolitana* and *C. saccharolyticus* monocultures

192 Hydrogen production by the hyperthermophiles *T. neapolitana* and *C.*
193 *saccharolyticus* was evaluated both as pure cultures and as a synthetic co-culture. For
194 the pure culture of *C. saccharolyticus*, a lag phase of 9 h was observed. The maximum
195 H₂ production rate obtained was 24.65 mL L⁻¹ h⁻¹. The growth obtained from OD
196 measurements reached a maximum OD_{600nm} of 0.66 (±0.03) (Figure 1). A decrease in
197 the OD was observed after glucose was completely consumed at 100 h suggesting that
198 the cultures entered death phase upon depletion of the carbon source. The H₂ yield
199 obtained was 2.7 (±0.05) mol H₂/mol glucose. Glucose consumption resulted in acetate
200 production with the absence of lactate formation (Figure 1). The absence of lactate in the
201 pure culture of *C. saccharolyticus* was likely as a result of a low partial H₂ pressure (P_{H₂})

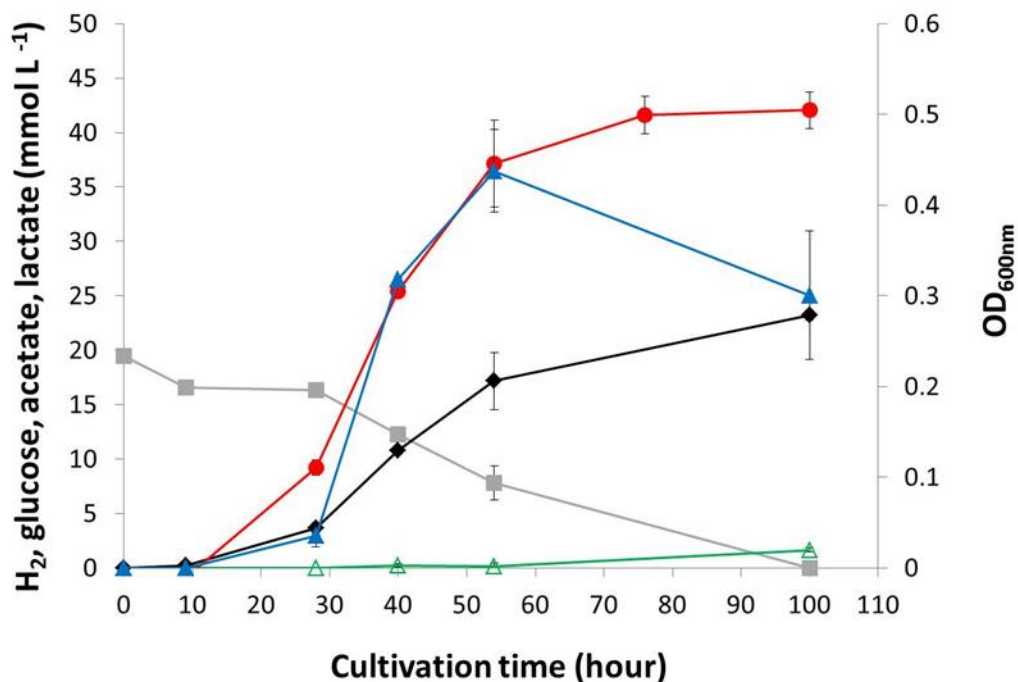
202 during the cultivations. A high P_{H_2} during dark fermentation is known to cause a shift in
203 the metabolic pathway.



204
205 Figure 1– Hydrogen production, glucose consumption, optical density (OD) of the
206 culture suspensions and soluble metabolites produced by *C. saccharolyticus* (●) H₂
207 production, (■) Glucose consumption, (△) Lactate, (◆) Acetate and (▲) OD. The error
208 bars represent the standard deviation from triplicate cultures. In some cases, the error
209 bars are smaller than the symbol.

210
211 Compared to *C. saccharolyticus*, *T. neapolitana* pure cultures had a longer lag
212 phase and the maximum H₂ production rate obtained was lower (15.51 mL L⁻¹ h⁻¹) than
213 in the synthetic co-culture or pure culture of *C. saccharolyticus*. The H₂ yield achieved
214 was 2.5 (±0.07) mol H₂/mol of glucose and compared to *C. saccharolyticus*, the

215 consumption of glucose was slower (Figure 2). Similar to *C. saccharolyticus* however,
216 the major metabolite formed was acetate. Lactate was also produced between
217 incubation time 60 h and 100 h. The OD values obtained for *T. neapolitana* were low
218 (0.44 ± 0.05) but this was expected due to the floc formation by the bacterium [28]. Prior
219 to OD measurements, vigorously shaking of the culture to disentangle the floc had little
220 impact on the cell density measurements. Though the growth pattern as measured by
221 the OD was similar to that obtained in *C. saccharolyticus*, the OD obtained was not
222 accurate enough to be considered in this study. Hence, an alternative molecular biology
223 based method was developed for accurate enumeration of *T. neapolitana*.



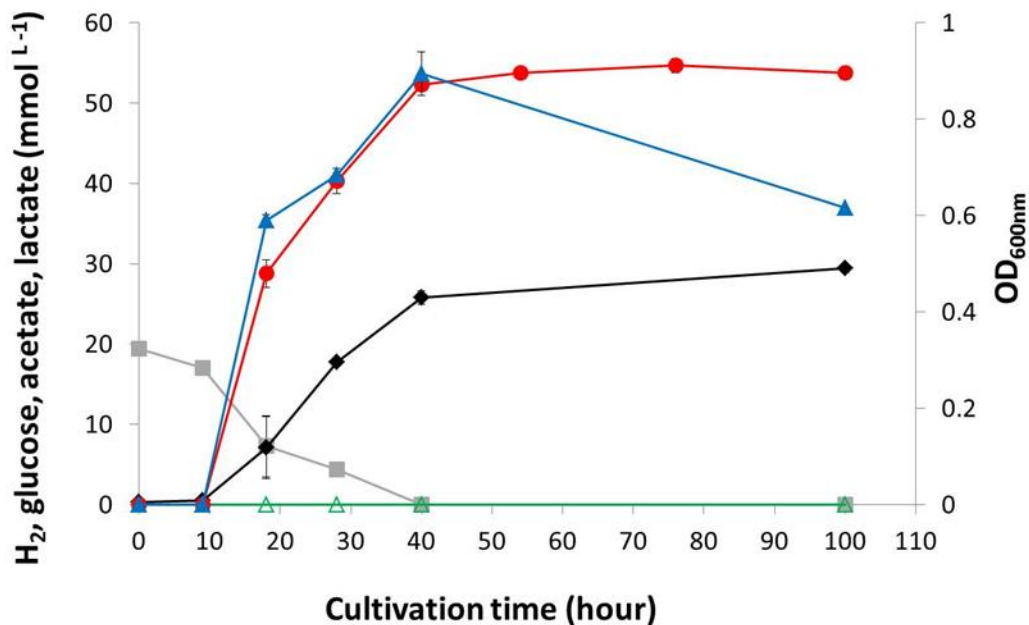
224
225 Figure 2– Hydrogen production, glucose consumption, optical density (OD) of the
226 culture suspensions and soluble metabolites produced by *T. neapolitana* (●) H₂
227 production, (■) Glucose consumption, (△) Lactate, (◆) Acetate and (▲) OD. The error

228 bars represent the standard deviation from triplicate cultures. In some cases, the error
229 bars are smaller than the symbol.

230

231 Results obtained for the synthetic co-cultures of *T. neapolitana* and *C.*
232 *saccharolyticus* showed that glucose was rapidly consumed compared to the pure
233 cultures (Figure 3). Similar to the pure cultures of *C. saccharolyticus*, a lag phase of 9 h
234 was observed and a maximum OD_{600nm} of 0.9 (± 0.04) was obtained during the
235 cultivation. The H₂ yield was 2.8 (± 0.09) mol H₂/mol of glucose. Compared to the
236 performance of the pure cultures, the synthetic co-cultures showed a clear improvement
237 in the H₂ production (Figure 3). The maximum H₂ production rate obtained was 36.02
238 mL L⁻¹ h⁻¹. Statistical analysis to compare the H₂ production rate of the synthetic co-
239 culture with either of the pure cultures gave a probability value of 0.15 ($p < 0.05$: t-test)
240 with *C. saccharolyticus* and 0.014 ($p < 0.05$: t-test) with *T. neapolitana* showing a
241 significant difference in the H₂ production rate.

242 Overall, the maximum hydrogen content in the pure cultures and the synthetic
243 co-culture was between 63% and 67%. Though *T. neapolitana* is able to form biofilm as
244 was observed in the pure culture, there was no biofilm formation observed when it was
245 cultivated with *C. saccharolyticus* as a synthetic co-culture. Cultivation of both
246 organisms also did not induce a shift in metabolic pathway as the major metabolite
247 produced was acetate. This therefore did not give a prediction on the interspecies
248 relationship that exists between both organisms. However, a more comprehensive study
249 to determine the relationship between both organisms will take into account the
250 differences in protein expression of the pure cultures and synthetic co-cultures.



251
 252 Figure 3– Hydrogen production by co-culture of *T. neapolitana* and *C.*
 253 *saccharolyticus* (●) H₂ production, (■) Glucose consumption, (△) Lactate, (◆) Acetate
 254 and (▲) OD. The error bars represent the standard deviation from triplicate cultures. In
 255 some cases, the error bars are smaller than the symbol.

256
 257 Several co-culture methods have been accessed for biohydrogen production
 258 under hyperthermophilic conditions and have been shown to be a promising strategy for
 259 improved H₂ production [35, 36]. Some extreme thermophilic bacteria such as,
 260 *Thermotoga maritima* and *C. saccharolyticus* are capable to hydrolyze polysaccharides
 261 and utilize the reducing equivalents formed during the glycolytic process for H₂
 262 production [38,39]. Additionally, *C. saccharolyticus* has been recognized as being
 263 relatively insensitive to H₂ partial pressure [40]. In this study, the results obtained with
 264 the synthetic co-culture showed improvements in H₂ production, suggesting a

265 synergistic effect between *T. neapolitana* and *C. saccharolyticus*. Compared to the pure
 266 strains, the co-cultures demonstrated a rapid glucose utilization and higher H₂
 267 production rate. The results obtained from this study is in line with the literature
 268 reporting enhanced H₂ production using synthetic co-cultures [36,38,41–46].

269
 270 Table 1. Comparison of biohydrogen production in hyperthermophilic co-cultures from
 271 different feedstocks and inoculum

Strain/co-culture	Substrate	Temperature (°C)	Maximum H ₂ yield (mol H ₂ /mol of glucose)	Reference
<i>C. saccharolyticus</i> and <i>T. maritima</i>	Xylose Cellobiose	70	2.7 ± 0.1	[38]
<i>C. Thermocellum</i> JN4 and <i>T. thermosaccharolyticum</i> GD17	Microcrystalline cellulose, cellobiose or filter paper	60	1.8 ± 0.09	[35]
<i>C. saccharolyticus</i> and <i>T. neapolitana</i>	Glucose	75	2.81 ± 0.09	This study

272

273 3.2. Specificity of *in silico* and experimental qPCR assays

274 In this study, quantitative monitoring of *Thermotoga* sp. was performed using
 275 real-time PCR and primers targeting the variable regions in *Thermotoga* 16S rDNA and
 276 *hydA* genes. The *hydA* gene has been used in quantitative monitoring of *Clostridium*
 277 *butyricum* in mesophilic hydrogen producing bioprocess systems [33,47]. The
 278 specificities of the newly designed primers were evaluated by *in silico* PCR of 16S rDNA
 279 primer and Primer-BLAST for both 16S rDNA and *hydA* primers. The *in silico* PCR
 280 analysis was conducted to include coverage of 613789 sequences that gave an output
 281 specific for members of the genus *Thermotoga* (Table 2).

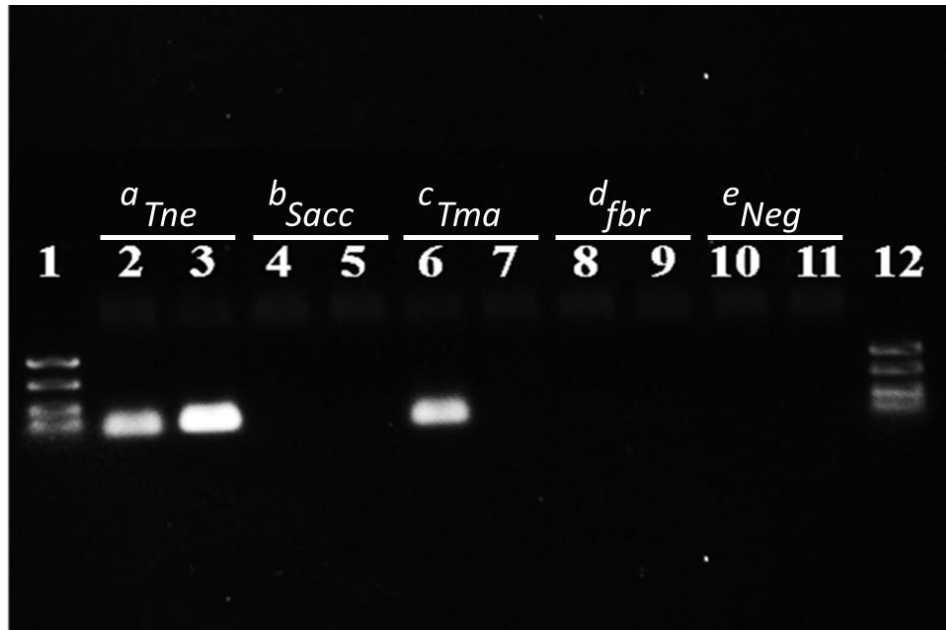
282

283 Table 2– 16S rDNA gene primer specificity towards *Thermotoga* sp. identified from *in*
284 *silico* PCR using arb-silva database.

Primary accession	Organism name	Start position	Stop position	Specificity (%)
CP000702	<i>Thermotoga petrophila</i>	753682	755234	100
CP000916	<i>Thermotoga neapolitana</i>	505958	507506	100
CP000969	<i>Thermotoga</i> sp. RQ2	788689	790242	100
CP001839	<i>Thermotoga naphthophila</i>	839610	841157	100
CP003408	<i>Thermotoga</i> sp. 2812B	793453	795015	100
CP003409	<i>Thermotoga</i> sp. Cell2	738805	740367	100
CP007633	<i>Thermotoga</i> sp. RQ7	783074	784640	100
CP010967	<i>Thermotoga maritima</i>	188967	190530	100

285

286 The overall sequence coverage by the primer obtained for the *in silico* PCR was
287 79.3%. Experimental evaluations for primer specificities were performed by qPCR with
288 melt curve analysis using target and non-target bacterial species as reference (*T.*
289 *neapolitana*, *T. maritima* and *C. saccharolyticus*, co-cultures of *T. neapolitana* and *C.*
290 *saccharolyticus* and mixed cultures from fluidized bed bioreactor). Since the 16S rDNA
291 amplicons had different lengths, the melt curve analysis for *T. neapolitana* and *T.*
292 *maritima* showed a slightly different melting temperature (T_m). However, the 16S rDNA
293 primers were specific towards *Thermotoga* sp. corroborating with the results predicted
294 by the *in silico* PCR. The *hydA* primers did not show any amplification with the reference
295 strains except with *T. neapolitana* which was the target organism (Figure 4). This
296 indicated the *hydA* primer's specificity towards *T. neapolitana*.

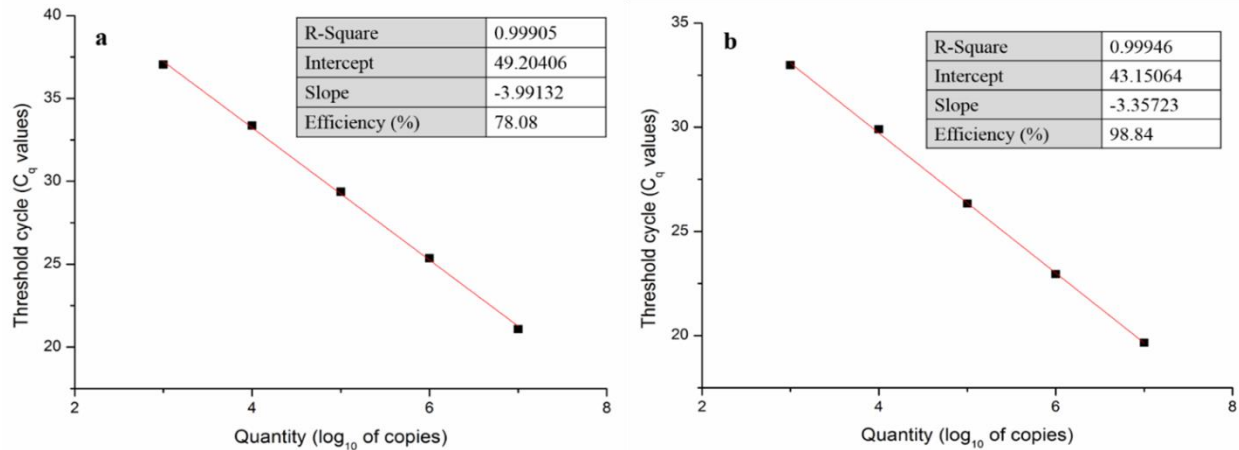


297

298 Figure 4– qPCR profile of *Thermotoga* sp. 16S rDNA and *T. neapolitana hydA*
 299 amplicons on agarose gel. (Lanes: 1 and 12= 1 kb GeneRuler DNA Ladder (Thermo
 300 Scientific, USA), lanes 2,4,6,8, and 10 were amplicons from 16S rDNA qPCR assay and
 301 lanes 3,5,7,9 and 11 were amplicons from *hydA* qPCR assay). *a*, *T. neapolitana*. *b*, *C.*
 302 *saccharolyticus*. *c*, *T. maritima*. *d*, fluidized bed bioreactor sample. *e*, Negative control
 303 without template.

304 3.3. Real-time quantitative PCR

305 The number of gene copies calculated from the constructed *T. neapolitana* 16S
 306 rDNA standard curve did not go beyond the defined value of 10^6 gene copies. The
 307 absolute cell number was calculated using equations 2 and 3, assuming that the genes
 308 of interest exist as a single copy in the genome [48,49]. The regression coefficients
 309 showed strong linear correlations for all targets during qPCR analysis (Figure 5).



310

311 Figure 5– Standard curve for *Thermotoga* 16S rDNA and *hydA* amplicons. Shown are:

312 a) *Thermotoga* sp. specific 16S rDNA amplicons and b) *T. neapolitana* *hydA* amplicons

313 with *T. neapolitana* genomic DNA as the template.

314

315 The amplification efficiencies of the designed real time qPCR primers were

316 evaluated using genomic DNA extracted from *T. neapolitana*. The reproducibility of both

317 primer pairs was determined with cultivation of *T. neapolitana* and the synthetic co-

318 culture (*T. neapolitana* and *C. saccharolyticus*). The standard curve from *T. neapolitana*

319 pure culture indicated amplifications efficiencies of 75% – 85% for 16S rDNA and 99%

320 for *hydA* (Figure 5) for each qPCR assay. Similar results on the primer specificities and

321 efficiencies were obtained when standards were run together with the synthetic co-

322 cultures. The qPCR data from the synthetic co-culture showed an increase in *hydA*

323 gene copies from 3.32×10^7 to 4.4×10^8 *hydA* gene copies per mL of sample during

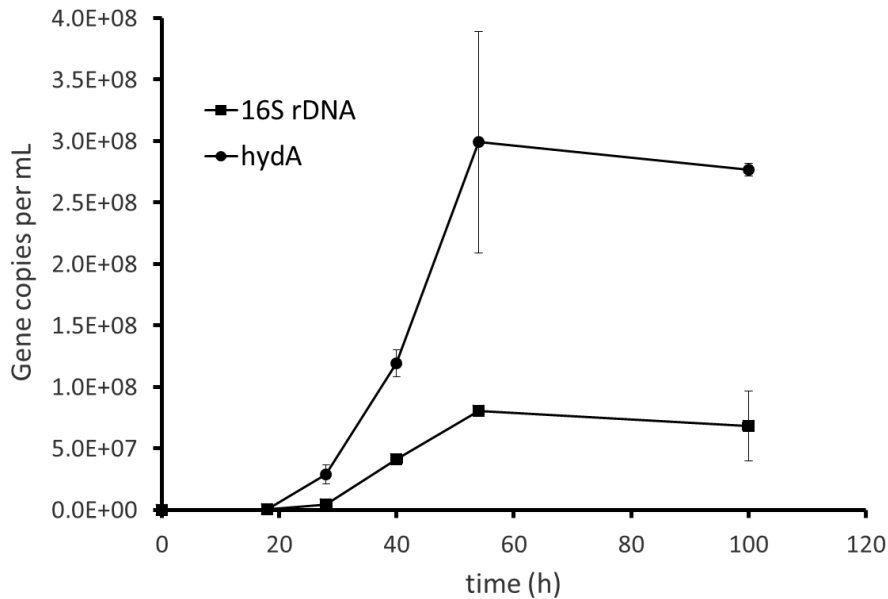
324 cultivation. This result proved that *T. neapolitana* in the synthetic co-culture had an

325 influence in the dark fermentation process. The 16S rDNA qPCR approach with the

326 same samples, under the same conditions showed a much lower number of gene

327 copies per mL of sample (Figure 6). This was suggested to be as a result of non-optimal

328 thermocycling condition. An *in silico* approach to optimize the 16S rDNA amplification
329 showed that increasing the annealing temperature from 60 °C to 72 °C had a significant
330 effect on the amplification efficiency.



331
332 Figure 5– Comparison of quantification results obtained from 16S rDNA and *hydA*
333 based approaches of *T. neapolitana* in synthetic co-culture. The error bars represent the
334 standard deviation from triplicate cultures. In some cases, the error bars are smaller
335 than the symbol.

336
337 Though the *hydA* primers demonstrated a considerably higher amplification
338 efficiency and sensitivity towards the target gene, both primers showed a similar
339 amplification pattern, confirming the specificity to their various targets. The molecular
340 method applied to this study facilitated to quantify and confirm the influence of *T.*
341 *neapolitana* in the H₂ production process. To the best of our knowledge, this is the first
342 report to demonstrate the application of *hydA* gene for species specific quantitative

343 monitoring of hyperthermophiles. Reports on biohydrogen production from
344 hyperthermophilic microorganisms have mostly utilized conventional methods for
345 monitoring the activity of the microbial population. Therefore, the molecular method
346 developed could be used as an alternative method in the cultivation of *Thermotoga* sp.
347 The quantitative analysis of *T. neapolitana hydA* in the synthetic co-culture showed an
348 increased number of *hydA* gene copies simultaneous to the hydrogen production
349 suggesting the growth of *T. neapolitana* in the co-culture culture. In a similar study, co-
350 cultivations of *C. saccharolyticus* and *T. maritima* [42] improved the hydrogen
351 production performance from simple sugars and complex substrates suggesting a
352 relationship of mutualism or commensalism. However, the kind of relationship that
353 exists in these systems and how beneficial it is for hydrogen production or metabolite
354 formation or the long term cultivation is still unknown and should be studied further.

355 One of the deterring factors for successful qPCR reaction is often tagged on the
356 efficiency of the designed primers. Studies on primer design, validation and usage in
357 microbial monitoring have used efficiencies ranging between 78% to 100% [33,34,47].
358 Factors such as amplicon length, melting temperature, annealing temperature and the
359 ΔG of the amplicon should always be taken into account. Using Mfold web server DNA
360 folding form prediction tool (<http://unafold.rna.albany.edu/?q=mfold/dna-folding-form>),
361 the ΔG value obtained for *Thermotoga* 16S rDNA and *hydA* amplicons at the qPCR
362 annealing temperature (60 °C) used in the experiment was calculated. There was a
363 significant variation in the 16S rDNA and the *hydA* (-14.69 kcal/mol and -0.09 to -0.7
364 kcal/mol, respectively). Given the values obtained for both target genes, it is probable
365 that the reason for the low efficiency obtained in 16S rDNA amplification was due to the

366 low ΔG value. The ΔG represents the quantity of energy needed to fully break a
367 secondary DNA structure and the lower the ΔG , the higher the quantity of energy that is
368 required to separate the DNA strands if self-dimers or hetero-dimers are formed. In
369 essence, higher temperatures are needed to break the dimer. When the folding
370 temperature of *Thermotoga* 16S rDNA amplicon sequence was increased to 72 °C *in*
371 *silico* (using the Mfold web server DNA folding form), a ΔG value of -8.80 kcal/mol was
372 obtained. With this value, the structure formed can be irrelevant in the qPCR reaction,
373 which means the efficiency could be improved by altering the annealing temperature.
374 Hence optimizing the thermocycling conditions can significantly influence the
375 amplification efficiency with the developed 16S rDNA primers. The high R-squared
376 values obtained in the 16S rDNA amplifications confirm that the reactions were
377 consistent with an absence of any non-specific product or primer dimer formation.
378 Overall, 16S rDNA and *hydA* based quantitative methods established were specific for
379 the genus *Thermotoga* and *T. neapolitana* respectively.

380 **CONCLUSIONS**

381 This study demonstrates that ecologically distant hydrogen producing organisms
382 with different cultivation conditions such as, *T. neapolitana* and *C. saccharolyticus*, can
383 be used for improvement of H₂ production yield and rate when cultivated as a synthetic
384 co-culture under optimized conditions. The co-cultures showed synergy such that there
385 was rapid substrate consumption and higher hydrogen production rate compared to the
386 respective monocultures. Additionally, qPCR methods were successfully developed for
387 genus and species specific quantitative monitoring of *Thermotoga* sp. in H₂ producing

388 systems. The *hydA* provided a promising target to complement with the existing 16S
389 rDNA gene-based methods for accurate monitoring growth and activity of *T. neapolitana*.
390 This study, therefore, offers a new avenue for research on simultaneous utilization of
391 pentose and hexose from various lignocellulosic waste materials for H₂ production by
392 the co-culture. Furthermore, the work presents an alternative quantification method for
393 genus-level monitoring of *Thermotoga* sp. and specie specific monitoring of *T.*
394 *neapolitana* which can be further explored for its ability to form biofilm and retain
395 biomass for improved hydrogen production under different cultivation conditions.

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