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8 **Comparison of *Scenedesmus acuminatus* and *Chlorella vulgaris* cultivation in**
9 **liquid digestates from anaerobic digestion of pulp and paper industry and**
10 **municipal wastewater treatment sludge**

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22 **Abstract:** Two microalgae, *Chlorella vulgaris* and *Scenedesmus acuminatus*, were batch
23 cultivated separately in two types of diluted liquid digestates. The first digestate (ADPP) was
24 obtained from a mesophilic laboratory digester treating biosludge from a pulp and paper industry
25 wastewater treatment plant. The second digestate (ADMW) was collected from a full-scale
26 mesophilic anaerobic digester treating mixed municipal wastewater treatment sludge. The highest
27 biomass production (as volatile suspended solids, VSS), 8.2–9.4 g L⁻¹, was obtained with *S.*
28 *acuminatus* in ADPP. *C. vulgaris* in ADMW had the lowest biomass production, reaching 2.0 g L⁻¹. Both microalgae removed ammonium efficiently from ADPP (99.9% removal rate) while the
29 final ammonium removal efficiencies from ADMW with *S. acuminatus* and *C. vulgaris* were only
30 44.0% and 23.8%, respectively. The phosphate removal efficiencies from both ADPP and ADMW
31 were higher than 96.9% with both microalgae. The highest carbohydrate content (60.5%) was
32 obtained with *S. acuminatus* cultivated in ADPP. *S. acuminatus* in ADPP showed one of the
33 highest biomass production yields that has been reported for microalgae in real wastewater-derived
34 nutrient sources. Consequently, this combination is promising for developing biorefinery and
35 biofuel applications in the pulp and paper industry.

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38 **Keywords:** microalgae; digestate; high biomass yield; nutrient removal; biorefinery

39 **1 Introduction**

40 The pulp and paper industry typically consumes large amounts of wood and water and is among
41 the largest producers of industrial wastewater in the world (Ashrafi et al. 2015). Thus, wastewater
42 treatment is an indispensable part of this industry. However, traditional aerobic wastewater
43 treatment produces vast amounts of biosludge, which is mechanically dewatered as such or mixed
44 with primary sludge and then typically incinerated or landfilled (Stoica et al. 2009). While
45 anaerobic digestion (AD) of the generated biosludge was studied in the 1980s (Puhakka et al. 1988),
46 the recent developments towards biorefineries and circular economy thinking have led to a
47 renewed interest in applying AD for biosludge treatment, as its energy balance is more positive
48 and it enables simpler nutrient recovery as compared to incineration (Kinnunen et al. 2015). A
49 microalgae-utilising biorefinery concept has been proposed to produce microalgae biomass and to
50 recover nutrients using the liquid effluent of pulp and paper mill-digested residue as a nutrient
51 source for the microalgae (Kinnunen and Rintala 2016; Kouhia et al. 2015). However, pulp and
52 paper mill wastewaters can contain compounds such as lignins, humic acids, furans and dioxins
53 (Ali and Sreekrishnan 2001), which can inhibit microbial growth and, thus, hinder utilisation of
54 the microalgal biomass for products such as biodiesel, biomethane and bioethanol, which require
55 large amount of biomass and cost-efficient cultivation. Microalgal cultivation in pulp and paper
56 mill digestates has been studied previously (Polishchuk et al. 2015; Kinnunen and Rintala 2016)
57 but resulted in low biomass production (0.2 g volatile suspended solids (VSS) per L) (Kinnunen
58 and Rintala 2016).

59 The cultivation of various microalgal species has been studied using various other waste streams
60 as well (Jia et al. 2016; Molinuevo-Salces et al. 2016; Nam et al. 2016; Posadas et al. 2016).
61 Municipal wastewater is one of the most often used wastewaters due to its large volumes and

62 accessible collection (Tan et al. 2015), and it has been shown to be promising for simultaneous
63 microalgal biomass production and nutrient recovery (Cai et al. 2013a; Tan et al. 2015). In addition
64 to studies on municipal wastewater, microalgae cultivation has also been studied using the liquid
65 fraction of the digestate from AD of municipal wastewater sludge. Tan et al. (2015) succeeded in
66 cultivating *Chlorella pyrenoidosa* outdoors using a diluted liquid fraction of anaerobically digested
67 biosludge, obtaining a maximum biomass concentration of 1.86 ± 0.09 g-VSS L⁻¹ during summer,
68 with the photobioreactor temperature ranging from 27.5 to 42.6 °C. This indicates the feasibility
69 of large-scale outdoor microalgal cultures using effluents from AD of sludges as a nutrient source.
70 However, the growth yields and nutrient recovery efficiency of different microalgal species can
71 be different, even under similar conditions (Abdel-Raouf et al. 2012), which makes it important to
72 find an optimal microalgal species for each application.

73 The aim of the present study was to assess the feasibility of cultivating microalgal biomass in pulp
74 and paper mill biosludge digestate. Utilising this concept, microalgae cultivation could be
75 integrated in pulp and paper industry biorefinery to produce microalgal biomass (e.g. to biofuel
76 applications while recovering nutrients from the liquid digestate). The digestate from a municipal
77 wastewater treatment plant was used as a reference cultivation medium. The cultivation of two
78 microalgal species, *Chlorella vulgaris* and *Scenedesmus acuminatus*, which were chosen due to
79 their high growth rates and yields as well as their broad use in wastewater treatment studies
80 (Bohutskyi et al. 2015; Wang et al. 2015; Zuliani et al. 2016), was compared in these two digestates.

81 **2 Materials and methods**

82 **2.1 Microalgal strains and growth medium for seed cultures**

83 *Chlorella vulgaris* (SAG 211-11b) and *Scenedesmus acuminatus* (SAG 38.81) were obtained from
84 the SAG Culture Collection of Algae at the University of Göttingen, Germany as culture
85 suspensions. *C. vulgaris* had been grown in Jaworski's medium (Lakaniemi et al. 2011) and stored
86 frozen at -85 °C for 4 years. After thawing, *C. vulgaris* was inoculated to 100 mL N-8 medium
87 and cultivated in 250 mL Erlenmeyer flasks on an orbital shaker (150 rpm) under fluorescent lamps
88 (Osram L 18W/965 bio lux, Germany) at a light intensity of 40 $\mu\text{mol photons m}^{-2} \text{ s}^{-1}$ as a seed
89 culture. *S. acuminatus* was inoculated to N-8 medium immediately after obtaining it from the
90 culture collection and cultivated under the same conditions as *C. vulgaris*. The N-8 medium
91 consisted of (g L^{-1}): KNO_3 , 0.5055; KH_2PO_4 , 0.7400; Na_2HPO_4 , 0.2598; $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.0500;
92 $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, 0.0175; $\text{FeNaEDTA} \cdot 3\text{H}_2\text{O}$, 0.0115 and micronutrient ($\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, 0.0032;
93 $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$, 0.013; $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$, 0.0183; $\text{Al}_2(\text{SO}_4)_3 \cdot 18\text{H}_2\text{O}$, 0.0070). The pH of the N-8
94 medium is naturally 6.5. *C. vulgaris* grew well with that initial pH, whereas there was no growth
95 of *S. acuminatus* in the N-8 medium with an initial pH of 6.5. Based on a previous study by Xu et
96 al. (2015), NaOH was added to adjust the pH to 8.0 for *S. acuminatus* cultivation.

97 **2.2 Digestates**

98 Digestates from two different sources were studied for microalgal growth. The first digestate
99 (ADPP) was collected from a mesophilic laboratory-scale (6 L) completely stirred tank reactor
100 (hydraulic retention time 14 d and organic loading rate 2.1 $\text{kgVS m}^{-3} \text{ d}^{-1}$) treating biosludge from
101 a pulp and paper industry wastewater treatment plant. The reactor set-ups were as described in
102 Kinnunen et al. (2015), but the biosludge used in this study originated from different pulp and
103 paper mills compared with the data reported in Kinnunen et al. (2015), and thus the digestate
104 characteristics are not directly comparable. The second digestate (ADMW) was collected from a

105 mesophilic anaerobic digester (typically operated at a hydraulic retention time of 20–25 d and
106 organic loading rate of 2.0 kgVS m⁻³ d⁻¹) treating mixed sludge in a municipal wastewater
107 treatment plant (Rahola, Tampere, Finland). The digestates were stored at 4 °C until prepared for
108 the cultivation experiments.

109 To remove particulate solids, both digestates were centrifuged at 5200 rpm for 4 min, and the
110 separated supernatant was filtered through a glass fibre filter (Whatman GF/A, UK) under non-
111 aseptic conditions (not meant to sterilise the wastewater). After filtration, the filtered digestates
112 were stored at 4 °C before use. This study includes two separate cultivation experiments with both
113 digestates. As the filtered digestates were prepared at different times and from different batches of
114 digestates for the two cultivation experiments (Experiments I and II), there were some differences
115 in the digestate compositions (Table 1). Considering that the PO₄³⁻-P level may be not sufficient in
116 ADMW, an additional experiment was performed with 0.548 g L⁻¹ K₂HPO₄ added to the ADMW
117 to enhance microalgal cultivation and nitrogen removal efficiency. Thus, the N/P ratio was
118 adjusted to 7.5, and this ratio was selected as it has been used for high nutrient removal during
119 microalgae cultivation in municipal wastewaters (Cai et al. 2013b; Tan et al. 2015).

120 **2.3 Microalgal cultivation in digestates**

121 Experiment I was done to select the optimal dilution factor of the liquid digestates for microalgal
122 growth. The digestates were diluted with distilled water, using dilution factors of 5x, 3x and 1.5x
123 and 10x, 7x, 3.5x, 2x and 1x for the ADPP and ADMW, respectively. Using the selected dilution
124 factors, Experiment II was conducted to further study the biomass production, carbon and nutrient
125 removal efficiency and chemical composition of the produced biomass (carbohydrate, lipid and
126 protein). All cultivations were performed in duplicates.

127 Experiment I was conducted in 1-L photobioreactors, which consisted of a 1-L glass bottle
128 (PYREX) closed with a plastic cap and having two tubes as the gas inlet and outlet. The cultures
129 were bubbled from the bottom with 5% CO₂ in the air (v/v) at a flow rate of 0.105 L min⁻¹ using a
130 glass distribution tube (porosity 0, ø 22mm, Duran Group, Germany). The photobioreactors were
131 continuously illuminated using white fluorescent lamps (Osram L 18W/965 De Luxe cool daylight,
132 Germany) from two sides of the reactors. It is commonly believed that each microalgal strain has
133 a particular light intensity that is the most optimal for biomass growth (Ho et al. 2012; Xu et al.
134 2015). Based on preliminary tests (data not shown) in which the microalgae were cultivated
135 separately in N-8 medium at different light intensities, 150 µmol photons m⁻² s⁻¹ and 240 µmol
136 photons m⁻² s⁻¹ were chosen as the light intensities for the cultivation of *C. vulgaris* and *S.*
137 *acuminatus*, respectively. The inoculum culture was centrifuged to separate cells from the N-8
138 medium before being mixed with the desired digestate. To identify the accurate microalgal growth
139 medium compositions in Experiment II, samples were taken for analysis of initial dissolved
140 nutrients after inoculation. Each microalgal genus was inoculated to its respective photobioreactor
141 to provide an initial optical density (OD) of 0.20. The initial total culture volume in the reactors
142 was 350 mL for ADPP (the availability was limited) and 700 mL for ADMW. The temperature of
143 the reactors was maintained at 22±2 °C. Distilled water was added to adjust for the water lost
144 through evaporation each time before taking samples for analyses. All cultivations (each
145 combination of different microalgal species with different dilution of digestate) were carried out
146 for 11–12 d.

147 Experiment II using the selected dilution factors was conducted using similar conditions as
148 Experiment I. The difference was that the initial culture volume in all the cultivations was 700 mL
149 to provide enough volume for the more extensive sampling and more reliable comparison of the

150 growth of the two microalgae in the two digestates. The cultivation duration in Experiment II was
151 14 d.

152 **2.4 Analyses and calculations**

153 The culture pH was measured using a WTW 3110 pH meter (WTW, Germany) with a SenTix[®] 41
154 electrode (WTW, Germany) in Experiment I and a WTW 330 pH meter (WTW, Germany) with a
155 Slimtrode electrode (Hamilton, Germany) in Experiment II. The light intensity was measured from
156 the outer surface of the photobioreactors by a MQ-200 Quantum Meter (Apogee, USA). The
157 optical density (OD) of the culture samples was measured at a wavelength of 680 nm using a
158 Shimadzu UV-1700 Pharmaspec spectrophotometer after proper dilution with deionised water to
159 give absorbance values between 0.2–0.7. Light microscopy was carried out using a Zeiss Axioskop
160 2 equipped with an AxioCam MRc camera. The microalgae cells were first sonicated for 10 min
161 and then observed under the light microscope. Volatile suspended solids (VSS) were measured by
162 filtering 5–15 mL culture solution through a glass fibre filter (Whatman GF/A). Each filter
163 containing the suspended solids was dried at 105 °C overnight, weighed and then burned in a 550
164 °C muffle furnace for 2 h and weighed again. VSS was determined gravimetrically as a difference
165 of the filters after treatment at these two temperatures. The filtrate from VSS filtration was used in
166 the analysis of soluble chemical oxygen demand (COD_s), dissolved organic carbon (DOC) and
167 nutrient (N, P) concentration.

168 COD_s was determined using the dichromate method according to the Finnish Standard SFS 5504.
169 DOC was measured with a total organic carbon analyser (Shimadzu Model TOC-5000) with an
170 ASI-5000 autosampler. Total nitrogen was measured as total Kjeldahl nitrogen (TKN) with the
171 Tecator Kjelttec Systems (FOSS Tecator Digestor 8 and KT 200 Kjelttec, Sweden), and total

172 phosphorus (TP) was measured with a Hach kit LCK349 (0.05–1.5 mg L⁻¹ PO₄-P) or LCK350
173 (2.0–20.0 mg L⁻¹ PO₄-P), according to the manufacturer’s instructions. NH₄⁺-N was measured with
174 an ion selective electrode (Thermo Scientific Orion ISE meter). The ammonium removal rate was
175 calculated as ARR=(C₀-C_t) t⁻¹, where C₀ is the ammonium concentration on day 0, and C_t is the
176 ammonium concentration when the ammonium concentration had fallen below 0.5 mg L⁻¹, which
177 indicated >99% NH₄⁺-N removal. The possible significance of ammonium stripping was estimated
178 by calculating the fraction of unionised ammonium with the following equation (Emerson et al.
179 1975) as rate of ammonia stripping has been shown to correlate well with free ammonia
180 concentration (Zimmo et al. 2003):

$$181 \quad \text{unionised } NH_3(\%) = \frac{100}{1 + 10^{(pK_a - pH)}}, \quad (1)$$

182 where $pK_a = 0.09018 + \frac{2729.92}{T}$ and T = temperature(°K).

183 NO₃⁻, NO₂⁻ and PO₄³⁻ were measured using an ICS-1600 ion chromatograph (Dionex, USA) with
184 an AS-DV autosampler, Ion- Pac AS4A-SC anion exchange column and ASRS-300 suppressor (2
185 mm). The eluent contained 1.9 mM Na₂CO₃ and 1.7 mM NaHCO₃, and the eluent flow rate was 1
186 mL min⁻¹.

187 The composition of the produced microalgal biomass (proteins, carbohydrates, and lipids) was
188 measured from the freeze-dried biomass. Before freeze-drying, the algal culture was centrifuged
189 at 5200 rpm for 2 min, and the supernatant was discarded. The harvested microalgae samples were
190 dried in a vacuum freeze dryer (Christ ALPHA 1-4 LD plus) for 24 h. The protein content of the
191 produced biomass was measured with a protein assay kit, based on the method of Bradford (Bio-
192 Rad Protein Assay Dye Reagent Concentration; Protein Standard II). The total carbohydrate
193 concentration of the algal biomass was measured with the anthrone method after hot alkaline
194 extraction (Chen and Vaidyanathan 2013). In short, 10 mg dried microalgal pellets were

195 resuspended in 0.2 mL distilled water and then heated in 0.4 mL 40% (w/v) KOH at 90 °C for 1 h.
196 After cooling down, the sample was mixed with 1.2 mL cold absolute ethanol and stored in a fridge
197 at –20 °C overnight. The pellet was resuspended in 1.5 mL distilled water after discarding the
198 supernatant. An aliquot (0.2 mL) of the sample was mixed and vortexed with 0.4 mL of pre-chilled
199 75% H₂SO₄ solution (stored at 4 °C) in a test tube. To this, 0.8 mL of the anthrone reagent (2 g L⁻¹
200 in 75% H₂SO₄, freshly prepared) was added, and then the mixture was subsequently boiled at
201 100 °C for 15 min. After cooling, the absorbance was read at 578 nm using a Shimadzu UV-1700
202 Pharmaspec spectrophotometer. The blank absorbance of the sample was read by reacting 0.2 mL
203 of the sample with 1.2 mL 75% H₂SO₄ without the anthrone reagent. The amount of carbohydrate
204 was estimated using a standard curve created using d-glucose. The total lipid content of the
205 biomass was measured by extracting the lipids with chloroform/methanol and determining the
206 lipids gravimetrically. An aliquot (50 mg) of freeze-dried microalgal biomass was mixed with 10
207 mL of chloroform/methanol (2/1, v/v) and then sonicated for 5 min. After sonication, the mixture
208 was reacted for 4 h on a magnetic stirrer at 1000 rpm. Then, 5 mL of distilled water were added to
209 the mixture and centrifuged together at 3000 rpm for 2–3 min. Lipids remained in the chloroform
210 after centrifugation, and then the chloroform (8 mL) was placed in a pre-weighted tube. The
211 nitrogen was sparged to remove chloroform for 2 h and lipid content was left in the tube; the tube
212 was then weighed again.

213 **3 Results**

214 **3.1 Selection of the dilution factor for the digestates**

215 The growth of *Chlorella vulgaris* and *Scenedesmus acuminatus* was tested with different dilutions
216 with the pulp and paper mill digestate (ADPP; 5x, 3x and 1.5x) and municipal sludge digestate

217 (ADMW; 10x, 7x, 5x, 3.5x, 2x and 1x) to study the growth of the two microalgae in the two
218 digestates at similar initial ammonium concentrations. As shown in Table 2, both *C. vulgaris* and
219 *S. acuminatus* had the highest biomass production in 2x diluted ADMW and 1.5x diluted ADPP.
220 Compared with the growth of both microalgae in ADMW, the biomass production in ADPP was
221 much higher (maximum VSS=9.4±0.8 g L⁻¹ of *S. acuminatus* and VSS=5.1±0.6 g L⁻¹ of *C.*
222 *vulgaris*). In fact, the obtained biomass production was among the highest reported for microalgal
223 cultivations that have been conducted in real wastewater (Table 3). The biomass production of
224 both microalgae was lower in undiluted ADMW, and it is likely that microalgal growth was limited
225 by the higher ammonium concentration (840 mg L⁻¹) and brownish colour of the undiluted
226 digestate. The initial ammonium concentrations in 2x diluted ADMW and 1.5x diluted ADPP were
227 420 mg L⁻¹ and 230 mg L⁻¹, respectively, whereas the corresponding phosphate concentrations
228 were 1.0 mg L⁻¹ and 16.0 mg L⁻¹, respectively. As the biomass production was the highest at these
229 conditions, 2x diluted ADMW and 1.5x diluted ADPP were selected for the more detailed study
230 of biomass production, nutrient removal and algal biomass composition in Experiment II.

231 **3.2 Algal growth and nutrient removal efficiency**

232 In Experiment II, the microalgal growth was studied in more detail using the selected dilutions
233 with both ADPP and ADMW. Of the two different digestates, both microalgae grew better in
234 ADPP when compared to ADMW and reached their highest biomass concentrations (*C. vulgaris*:
235 2.9 g L⁻¹; *S. acuminatus*: 8.2 g L⁻¹) on day 14 (Fig. 1a). In ADMW, *S. acuminatus* reached a
236 maximum biomass concentration of 2.9 g L⁻¹ and *C. vulgaris* of 2.0 g L⁻¹. The biomass
237 concentration of *S. acuminatus* in ADPP was higher than that detected for the other cultivations
238 from day 2 onwards. On day 7, the biomass concentration of *S. acuminatus* in ADPP was already

239 4.9 g L⁻¹, while in the other cultivations biomass concentrations remained below 3.0 g L⁻¹ on day
240 14.

241 Both microalgae were able to remove ammonium efficiently from ADPP, in which the ammonium
242 concentration decreased from 240 mg L⁻¹ to 0.1 mg L⁻¹ during cultivation of both microalgal
243 species, resulting in a 99.9% removal efficiency (Fig. 2b). Interestingly, the same amount of
244 ammonium and phosphorus was removed by both algae in ADPP, even though the biomass
245 production for *S. acuminatus* (8.2 g L⁻¹) was more than two times higher than that for *C. vulgaris*
246 (2.9 g L⁻¹). The ammonium was, however, removed faster by *S. acuminatus* (26.5 mg L⁻¹ d⁻¹) than
247 by *C. vulgaris* (17.1 mg L⁻¹ d⁻¹). From ADMW, which had an initial ammonium concentration of
248 410 mg L⁻¹, the ammonium removal efficiencies were much lower, being only 44.0% and 23.8%
249 with *S. acuminatus* and *C. vulgaris*, respectively (Fig. 1b).

250 The initial phosphate concentration in ADPP was 8.0 mg L⁻¹ while in ADMW it was much lower
251 (1.3 mg L⁻¹, Fig. 1c), apparently due to phosphorus removal using chemical precipitation in the
252 municipal wastewater treatment plant. The phosphate levels in ADPP and ADMW decreased
253 rapidly to below the detection limit of 0.1 mg L⁻¹ by both microalgae, in 4 days with ADPP and 2
254 days with ADMW. Thus, the phosphate removal efficiencies were higher than 96.9% in all four
255 cultivations (Fig. 1c). An additional experiment performed to assess the effects of phosphate
256 addition to the ADMW (initial phosphate concentration was 73.8±1.8 mg L⁻¹, added as K₂HPO₄)
257 resulted in 99% removal of phosphate within 9 days with *S. acuminatus* and 14 days with *C.*
258 *vulgaris* but similar biomass production and ammonium removal efficiency as cultivations without
259 extra phosphate (Fig. 1).

260 **3.3 COD and DOC during microalgal cultivation in the digestates**

261 It is essential to measure COD in wastewater treatment, as it is a typical indicator of the water
262 quality. The initial COD_s value in the 2x diluted ADMW was 1259±5 mg L⁻¹, which was
263 approximately two times the initial value present in the 1.5x diluted ADPP having COD_s of 600±34
264 mg L⁻¹. In ADPP, the COD_s removal efficiencies of *C. vulgaris* and *S. acuminatus* were 27.6%
265 and 36.1%, respectively (Fig. 2a). In ADMW, the highest COD_s removal efficiency was obtained
266 with *C. vulgaris* (55.4%), while *S. acuminatus* was able to remove 48.7% of the initial COD_s. DOC
267 is a typical parameter measured from microalgal cultivations, as DOC is usually released during
268 microalgal photosynthesis and can support bacterial growth (Watanabe et al. 2005; Hulatt and
269 Thomas 2010). The DOC concentration in ADPP was stable and remained close to the initial value
270 during the whole cultivation period (Fig. 2b). A similar amount of DOC was removed from
271 ADMW by the two microalgae (26.0% by *C. vulgaris*, 24.8% by *S. acuminatus*) (Fig. 2b).

272 **3.4 Chemical composition and morphological changes of the microalgae**

273 Among all studied cultures, *S. acuminatus* in ADPP had the highest carbohydrate content (60.5%)
274 per dry weight, whereas a carbohydrate content of only 6.8% was measured from the dried cells
275 of *C. vulgaris* cultivated in ADPP (Table 3). Similarly, the carbohydrate content of *S. acuminatus*
276 and *C. vulgaris* grown in ADMW were 44.3% and 6.3%, respectively.

277 *C. vulgaris* is spherical in shape while *S. acuminatus* is spindle-shaped (Fig. 3). No morphological
278 differences in the *C. vulgaris* cells in the two digestates were observed between day 4 and day 14
279 (these cultivation days represent nitrogen-sufficient and nitrogen-limited conditions in ADPP).
280 The cell size (diameter) of *C. vulgaris* was about 5–10 µm in both studied digestates during the
281 whole cultivation period. However, clear morphological changes of *S. acuminatus* were detected
282 in both digestates between day 4 and day 14. In ADPP, the cell length of *S. acuminatus* increased

283 from 20 to 22.5 μm on average while the width increased from 6.25 to 7.5 μm on average. In
284 ADMW, the cell length of the *S. acuminatus* decreased from an average of 30 to 25 μm while the
285 width increased from an average of 8.75 to 11.25 μm . Slightly different types of changes in cell
286 morphology were observed in a previous study, in which the cell length size of *Scenedesmus* sp.
287 was found to increase from 4.5 to 5.3 μm while the cell width size decreased from 3.36 to 2.44 μm
288 when cultivated under a nitrate-limited condition (Pancha et al. 2014). Thus, there was no clear
289 correlation between nitrogen availability and the cell size.

290 **4 Discussion**

291 This study was carried out in batch to select microalgal species that enable high biomass
292 production and efficient nutrient removal from pulp and paper mill biosludge digestate and to
293 assess the potential of pulp and paper mill biosludge digestate as a cultivation medium compared
294 to the more commonly used municipal wastewater treatment digestate. The biomass production of
295 *S. acuminatus* cultivated in ADPP (8.2–9.4 g L^{-1}) in this study was among the highest obtained
296 when microalgae have been cultivated in real wastewater, while several studies have reported high
297 microalgal biomass production (7.22–12.4 g L^{-1}) in artificial growth medium (Table 3).

298 The selection of medium dilution plays an important role in microalgal cultivation since the
299 dilution will change the medium turbidity (thus light penetration) and nutrient concentrations
300 (Posadas et al. 2016; Wang et al. 2010; Xia and Murphy 2016). High ammonia concentrations
301 have been shown to inhibit microalgal growth, whereas too low nutrient concentrations can limit
302 growth (Britto and Kronzucker 2002; Tan et al. 2015). In contrast to our study, Franchino et al.
303 (2013) chose higher dilution ratios (1:10, 1:15, 1:20 and 1:25) as optimum to ensure the microalgal
304 growth due to the high digestate medium turbidity. However, higher dilutions reduced the

305 concentrations of nutrients, which could result in lower microalgal biomass production (Franchino
306 et al. 2013; Wang et al. 2010). Instead of clean water, Bohutskyi et al. (2016) mixed 1–20%
307 anaerobic digestion centrate (ADC) with primary and secondary wastewater effluents separately
308 to cultivate several types of microalgal strains, and they found that 5–10% ADC succeeded in
309 improving microalgal growth and productivity in both effluents due to the additional nutrients and
310 optimum nitrogen-to-phosphorus ratio.

311 The present study shows a high microalgal biomass yield is possible in the liquid digestates from
312 pulp and paper wastewater treatment plant biosludge. The growth of *S. acuminatus* appeared to be
313 similar level in both ADPP (8.2–9.4 g-VSS L⁻¹) and ADMW (2.2–2.9 g-VSS L⁻¹) in Experiment I
314 and II, while *C. vulgaris* growth differed more between the two experiments, with both digestates
315 being higher in ADPP in Experiment I (5.1 vs. 2.9 g-VSS L⁻¹) and in ADMW in Experiment II
316 (2.0 vs. 1.2 g-VSS L⁻¹). Even though a strict comparison between the two cultivations is not
317 justified due to different sampling dates and slightly different cultivation conditions, this shows
318 the repeatability of the high biomass production of *S. acuminatus* in ADPP. On the other hand, the
319 growth of *C. vulgaris* appeared to be more sensitive to cultivation conditions even when including
320 the differences in the compositions of the digestates in Experiments I and II (Table 1). Similarly,
321 in the previous study, the growth of *C. vulgaris* has been found to vary (0.31–0.19 g-VSS L⁻¹)
322 when using even synthetic growth medium (Kinnunen and Rintala 2016).

323 Several possible reasons (e.g. algal species, medium characteristics and microbial community)
324 could explain the different growth yields in the cultivations of this study. Kinnunen and Rintala
325 (2016) obtained a concentration of 0.17 g L⁻¹ (VSS) when *Scenedesmus sp.* was cultivated in a
326 liquid digestate from a different pulp and paper mill. The growth of this different *Scenedesmus*
327 species was much lower than the biomass production obtained with *S. acuminatus* in ADPP in this

328 study. Lignin, which ends up in pulp and paper mill wastewaters, is an amorphous polymer that is
329 difficult for microorganisms to degrade (Higuchi 1990). In addition, some of the polyphenolic
330 compounds in softwood knots, such as pinosylvins, have antimicrobial activity (Välilmaa et al.
331 2007), while lignin and its derivatives are quite toxic to certain microorganisms, such as
332 microalgae and cyanobacteria (Ball et al. 2001). It has been reported that *S. subspicatus* was much
333 more resistant than *C. vulgaris* and *Microcystis aeruginosa* to the chemicals released from barley
334 straw (e.g. 2 phenyl-phenol, p-cresol and benzaldehyde) (Murray et al. 2010). This indicates that
335 *C. vulgaris* was more susceptible to the chemical compounds likely present in ADPP, which may
336 have caused the much lower biomass production obtained with *C. vulgaris* than with *S. acuminatus*
337 in ADPP. When microalgae are cultivated in wastewaters or digestates, microbes are always
338 present and might affect the growth of microalgae. In the present study, the indigenous microbial
339 communities of the two digestates (ADPP and ADMW) were likely different since they originated
340 from different types of sources and had very different chemical compositions. Studies have shown
341 that certain bacteria can enhance bacterial growth, whereas certain bacteria can inhibit it (Croft et
342 al. 2005; Santos and Reis 2014). For example, De-Bashan et al. (2004) reported that *Azospirillum*
343 *brasilense* strain Cd stimulated the growth of *C. vulgaris* and *C. sorokiniana* when they were co-
344 immobilised in small alginate beads. Interestingly, a similar genus, *Azospirillum lipoferum*, was
345 found in an aerated plug-flow lagoon that was used to treat pulp and paper mill effluent (Yu and
346 Mohn 2001). However, De Bashan et al. (2004) did not study the effect of *Azospirillum brasilense*
347 on *S. acuminatus*, and therefore it is not possible to compare the effect of *Azospirillum* to the
348 growth of *C. vulgaris* and *S. acuminatus*. Lee et al. (2016) assumed that the reason for the slow
349 growth of *S. quadricauda* in municipal wastewater might be related to *Alcaligenes*, which was an
350 abundant bacterium in the wastewater. Some species of *Alcaligenes* genus have been shown to

351 cause cell lysis and the death of certain cyanobacteria (Manage et al., 2000), and others have been
352 shown to have nitrification and denitrification abilities that may affect ammonium removal and
353 nitrogen availability to the microalgae (Joo et al. 2005). The interactions between bacteria and
354 microalgae have been shown to be very species specific, even in the same medium (Schäfer et al.
355 2002). In our study, certain a bacterium present in the studied ADPP may have enhanced the
356 growth of *S. acuminatus* but not the growth of *C. vulgaris*. Alternatively, a certain bacterium could
357 have inhibited *C. vulgaris* but not *S. acuminatus*.

358 The present results demonstrate efficient nutrient (ammonium and phosphorus) removal by both
359 microalgae from ADPP, while different nutrient removal efficiencies were obtained in ADMW
360 with the two different microalgal strains. Beuckels et al. (2015) reported that *C. vulgaris* was able
361 to accumulate more nitrogen into biomass than *S. obliquus*. This likely happened in this study with
362 ADMW, as the decrease in $\text{NH}_4^+\text{-N}$ concentration was higher with *C. vulgaris* than with *S.*
363 *acuminatus* (Fig. 1b), although the biomass growth of *C. vulgaris* was somewhat lower (Fig. 1a).
364 Several possible ammonium transformations (algal uptake, ammonia stripping, bacterial growth
365 and nitrification) can happen in algae–bacteria consortium systems, such as microalgal cultures in
366 unsterilised wastewater (Bohutskyi et al. 2015; González-Fernández et al. 2011; He et al. 2013;
367 Zimmo et al. 2003). In this study, the nitrate and nitrite levels in both liquid digestates were low
368 ($<1.0 \text{ mg L}^{-1}$) during the whole cultivation. This means the possibility of ammonium removal by
369 nitrification was small. As the pH varied in all cultures between 7.5 and 8.0 and the average
370 temperature was 22°C , the theoretical fraction of unionised ammonia in all cultivations was 1.4%–
371 4.4%. This suggests that some stripping of the unionised ammonia may have occurred but that the
372 main portion of the removed ammonium from the digestates was used for microbial growth. The
373 removed phosphorus could be taken up into the microalgal cells as polyphosphates and/or cell

374 components or precipitate from the medium due to high pH (Cai et al. 2013a, b). Thus, it seems
375 that the higher initial phosphate concentration of ADPP was not the reason for the higher biomass
376 production observed in ADPP than in ADMW.

377 While there was no big difference in DOC removal with *C. vulgaris* and *S. acuminatus* when the
378 same digestate was used, the difference in DOC trends between ADPP and ADMW emphasise
379 their differences as a cultivation medium. One reason for stable DOC in ADPP could be that the
380 released DOC from photosynthetic microalgal cells equalled to the consumed DOC for growth of
381 heterotrophic organisms (such as bacteria). Decrease in COD_s suggests, however, that higher level
382 of organic compounds was degraded during the cultivation than was released as DOC by the
383 microalga. COD_s was not fully removed during the cultivations, indicating that treatments other
384 than biological methods could be required for further COD_s removal after microalgal harvesting.

385 The nutrient and carbon removal levels from ADPP were similar with both *C. vulgaris* and *S.*
386 *acuminatus*, but the biomass production of *S. acuminatus* was much higher than that of *C. vulgaris*.
387 Based on the typical biochemical composition of microalgae, it is estimated that about 50% of the
388 microalgal biomass is carbon (Chisti 2008). Thus, 1.0–4.1 g L⁻¹ carbon was required to produce
389 the microalgal biomass, as the obtained VSS values ranged between 2.0 and 8.2 g L⁻¹ for the two
390 microalgae (Fig. 1a). However, the total removed dissolved carbon from the digestates was below
391 150 mg L⁻¹. Hence, CO₂ supply contributed to the microalgal growth as the main carbon source,
392 indicating that most of the microalgal biomass was produced via photoautotrophic growth.

393 Based on the chemical formulas of the main components of microalgae (carbohydrate: C₆H₁₀O₅,
394 lipid: C₅₇H₁₀₄O₆ and protein: C_{1.9}H_{3.8}ON_{0.5}P_{0.031}) (Kouhia et al. 2015), nitrogen only appears in
395 proteins. It is assumed that microalgae using the same amount of nitrogen should produce the same
396 amount of protein. However, in this study, despite the similar ammonium removal, the protein

397 content of *C. vulgaris* was 6–13.8 percentage units higher than that of *S. acuminatus* in the same
398 digestate, whereas *S. acuminatus* contained significantly more carbohydrates and produced more
399 biomass than *C. vulgaris*. Nitrogen deficiency can cause a reduction in protein content (Diniz et
400 al. 2016) along with an enhancement of energy-rich products, such as carbohydrates and lipids (de
401 Farias Silva and Bertucco 2015; Siaut et al. 2011). In this study, the produced microalgal biomass
402 likely contained mainly proteins at the beginning due to the sufficient nitrogen in the cultures, and
403 the microalgal carbon was allocated to energy-rich compounds after the ammonium was consumed
404 completely. Similarly, when microalga *Chlamydomonas reinhardtii* was exposed to environmental
405 stress such as nitrogen starvation, starch accumulation was first observed and reached high levels
406 by day 2 (approximately 60 µg per million cell), and after extended nitrogen limitation (5 days),
407 oil accumulation reached a maximal level (40 µg per million cell) (Siaut et al. 2011). The
408 carbohydrate and lipid contents of *C. vulgaris* in ADMW and ADPP were in a similar range, while
409 the protein content of *C. vulgaris* in ADMW was higher than that in ADPP (Table 3), likely due
410 to the higher initial nitrogen concentration of ADMW compared to that of ADPP. However, as the
411 sum of the analysed biochemical components (58.8%–71.1%) from *C. vulgaris* was much lower
412 than 100%, it is not certain whether carbohydrate or lipid accumulation occurred in *C. vulgaris*.
413 The sum of proteins, lipids and carbohydrates in *C. vulgaris* has also been reported to be lower
414 than 70% in previous studies (Lakaniemi et al. 2011; Sydney et al. 2010). Burczyk et al. (2014)
415 suggested that low levels of polyamines (PAs) in the cell walls of microalgae might enhance the
416 action of lytic enzymes, and they found that the PA content in *C. vulgaris* strain 140 was 4 to 5
417 times higher than that in *S. obliquus* strain 633. Thus, it is possible that in this study and also in
418 the previous studies reporting sums of proteins, carbohydrates (sugars) and lipids to be clearly
419 below 100%, the high PA content in *C. vulgaris* may have hindered the cell lysis during the

420 analysis of the biochemical components. In addition, carbohydrates might have been lost due to
421 the alkali dissolution during the measurement (Kane and Roth 1974).

422 **5 Conclusion**

423 *Chlorella vulgaris* and *Scenedesmus acuminatus* were shown to be able to grow and remove
424 nutrients in liquid digestates from both a pulp and paper industry wastewater treatment plant
425 (ADPP) and a municipal wastewater treatment plant (ADMW). *S. acuminatus* in 1.5-times diluted
426 ADPP enabled the highest biomass production of 8.2–9.4 g L⁻¹, which is among the highest yields
427 reported for microalgae cultivated in wastewaters. The maximum biomass yield was also much
428 higher than the growth of *C. vulgaris* in 1.5-times diluted ADPP (2.9 g L⁻¹) as well as the growth
429 of *S. acuminatus* (2.9 g L⁻¹) and *C. vulgaris* (2.0 g L⁻¹) in 2-times diluted ADMW. Phosphate and
430 ammonium removal efficiencies were high with both microalgae from ADPP (over 97%). Both
431 algae were able to remove phosphate from ADMW, although the ammonium removal efficiencies
432 remained low (24–44%). According to the results obtained in this study, cultivation of *S.*
433 *acuminatus* in pulp and paper mill biosludge digestates is a promising approach for producing a
434 carbohydrate-rich biomass with a high yield and cheap nutrient supply (e.g. for biogas and
435 bioethanol production). Future studies on semi-continuous or continuous cultivation systems and
436 biomass harvesting could further promote the practical applications.

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592 **Figure captions:**

593 **Fig. 1** Microalgal biomass concentration (as g VSS L⁻¹) (a), the soluble ammonium-N (b) and
594 phosphate-P concentrations (c) during the cultivation of *Chlorella vulgaris* and *Scenedesmus*
595 *acuminatus* in the digestates from the pulp and paper wastewater treatment plant (ADPP; 1.5x
596 diluted), the municipal wastewater treatment plant (ADMW; 2x diluted) and the municipal
597 wastewater treatment plant supplied with phosphorus (ADMW+phos.; 2x diluted). The results of
598 VSS and phosphate-P are presented as the means of n = 4 (2 cultivations, 2 measurements from
599 each); error bars represent standard deviation. The results of ammonium-N are presented as the
600 means of n = 2 (2 cultivations, 1 measurements from each); error bars represent standard error.

601 **Fig. 2** COD removal efficiency (a) and DOC concentration (b) during the cultivation of *Chlorella*
602 *vulgaris* and *Scenedesmus acuminatus* in the digestates from the pulp and paper wastewater
603 treatment plant (ADPP; 1.5x diluted) and the municipal wastewater treatment plant (ADMW; 2x
604 diluted). The results are presented as the means of n = 4 (2 cultivations, 2 measurements from
605 each); error bars represent standard deviation.

606 **Fig. 3** Microscope photos of the microalgal cells: *Chlorella vulgaris* in ADPP (a)(c); *Chlorella*
607 *vulgaris* in ADMW (b), (d); *Scenedesmus acuminatus* in ADPP (e), (g) and *Scenedesmus*
608 *acuminatus* in ADMW (f), (h) on day 4 and day 14, respectively. Digestates were from the pulp
609 and paper wastewater treatment plant (ADPP; 1.5x diluted) and the municipal wastewater
610 treatment plant (ADMW; 2x diluted)

611

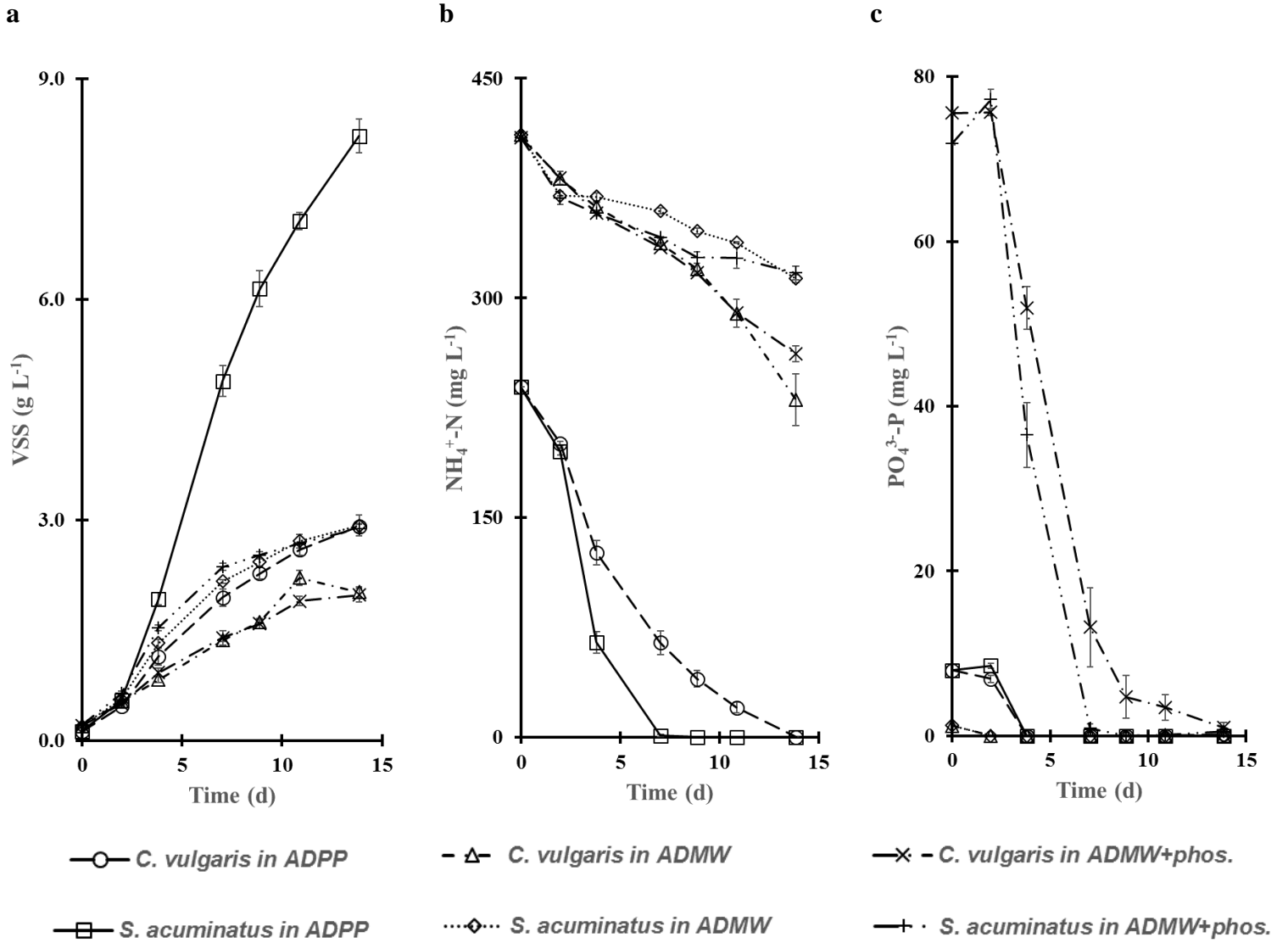
612 **Table captions:**

613 **Table 1** Characteristics of the filtered digestates originating from the pulp and paper wastewater
614 treatment plant (ADPP) and the municipal wastewater treatment plant (ADMW). Two batches
615 (Experiment I and II) of both filtered digestates were used. The results are presented as the means
616 of $n = 2$ (2 cultivations, 1 measurements from each); error bars represent standard error

617 **Table 2** Ammonium-N and phosphate-P concentrations and biomass production of *Chlorella*
618 *vulgaris* and *Scenedesmus acuminatus* cultivated in diluted digestates from a pulp and paper mill
619 wastewater treatment plant (ADPP) and a municipal wastewater treatment plant (ADMW). The
620 results of biomass production as the means of $n = 4$ (2 cultivations, 2 measurements from each);
621 error bars represent standard deviation. The results of ammonium-N and phosphate-P are presented
622 as the means of $n = 2$ (2 cultivations, 1 measurements from each); error bars represent standard
623 error

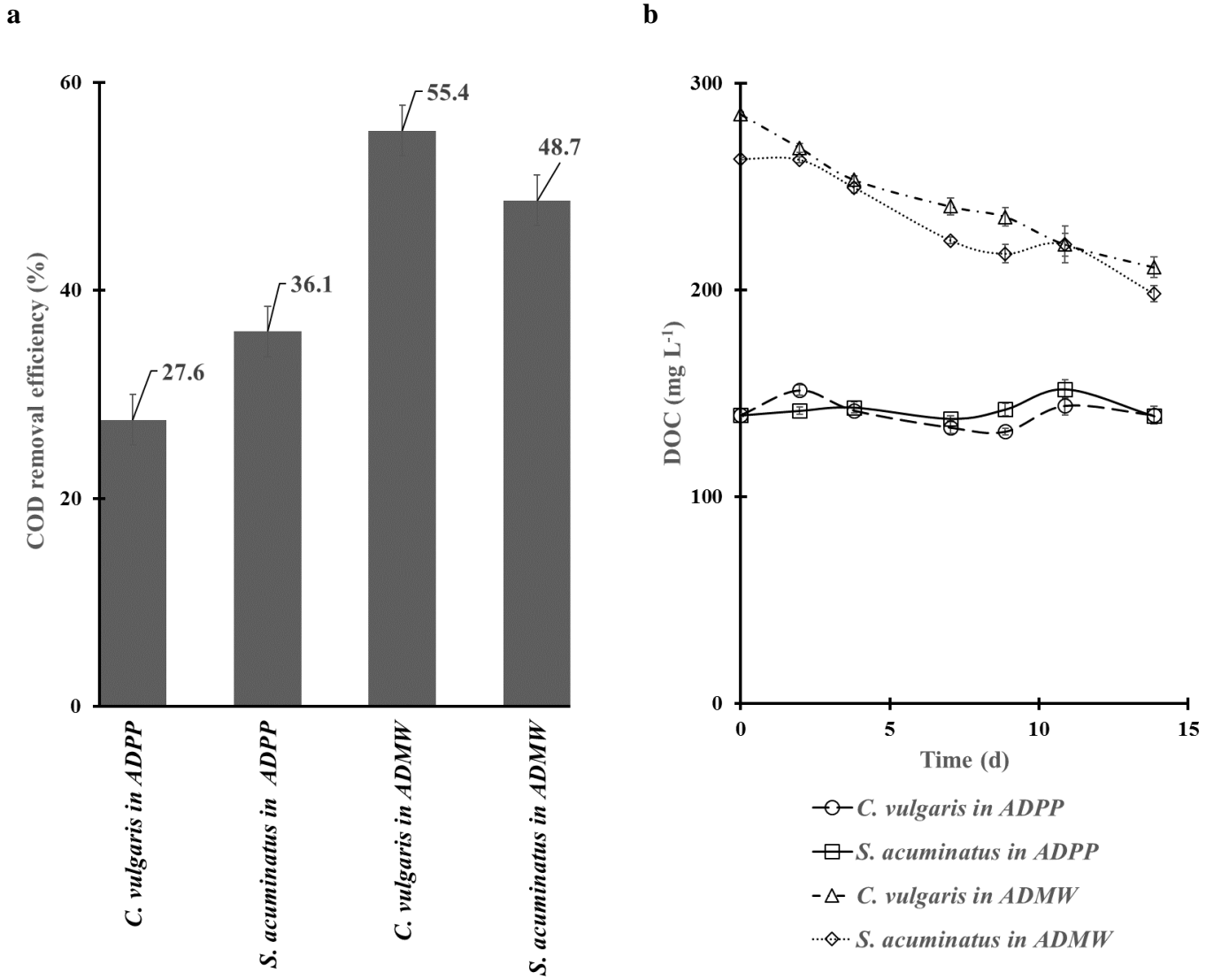
624 **Table 3** Maximum biomass concentrations and chemical compositions of the produced biomass
625 from selected studies in which microalgae have been cultivated in real wastewaters and synthetic
626 media. The digestates were from the pulp and paper wastewater treatment plant (ADPP; 1.5x
627 diluted) and the municipal wastewater treatment plant (ADMW; 2x diluted)

628 **Figure 1**

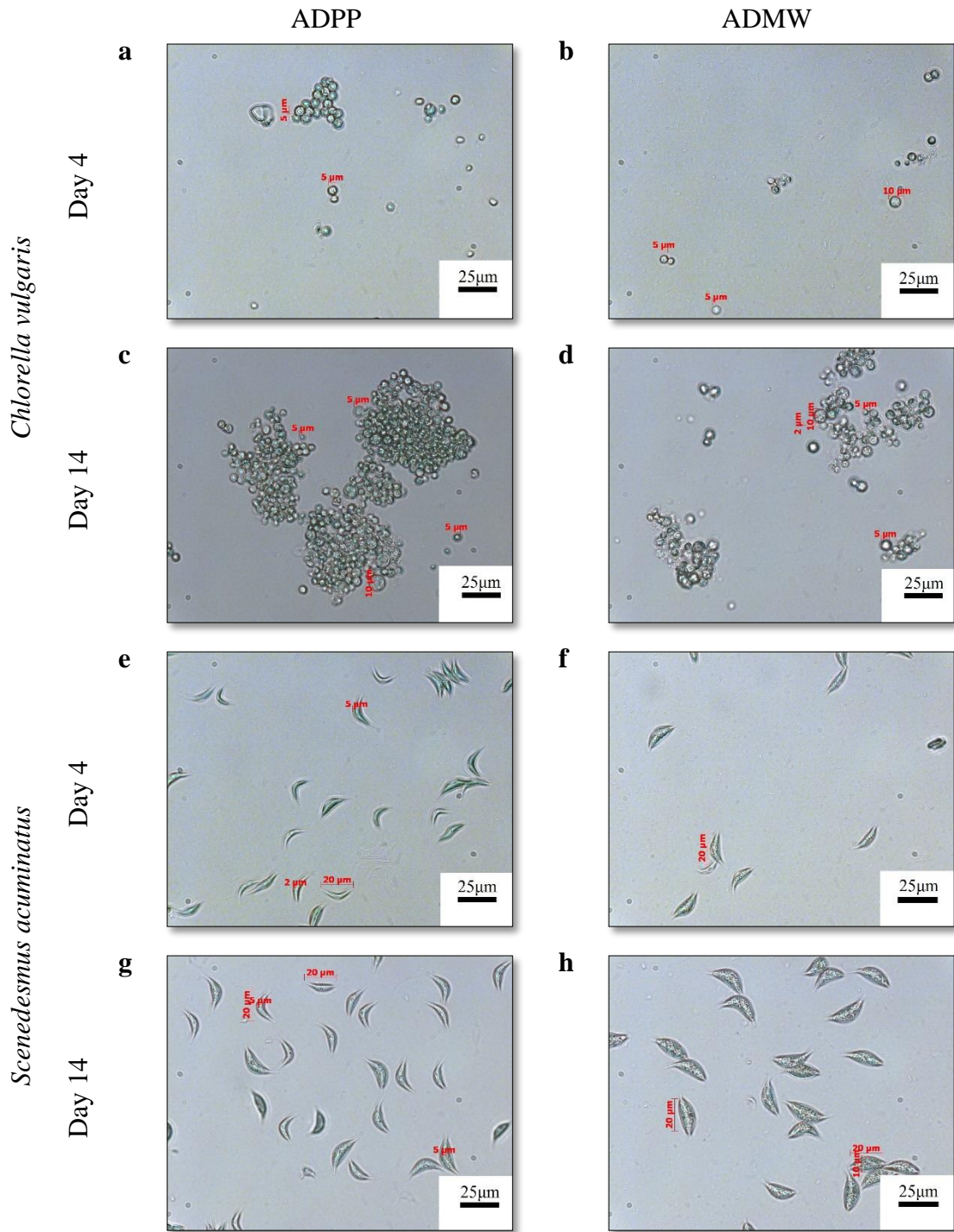


629

630 **Figure 2**



631



634 **Table 1**

	ADPP		ADMW	
	Experiment I	Experiment II	Experiment I	Experiment II
pH	8.5	8.5	8.3	8.6
DOC (mg L ⁻¹)	370±40	210±2	530±20	560±20
COD _s (mg L ⁻¹)	910±30	900±70	1850±40	2500±15
TKN (mg L ⁻¹)	350±10	360±20	840±40	1000±150
NH ₄ ⁺ -N (mg L ⁻¹)	350±50	360±1	840±130	820±10
NO ₃ ⁻ (mg L ⁻¹)	<0.5	<0.5	<0.5	<0.5
NO ₂ ⁻ (mg L ⁻¹)	<0.5	<0.5	<0.5	<0.5
TP (mg L ⁻¹)	28±1	20±1	10±1	14±2
PO ₄ ³⁻ -P (mg L ⁻¹)	24±1	12±0.1	2.0±0.2	2.5±0.1

635 DOC= dissolved organic carbon

636 COD_s = soluble chemical oxygen demand

637 TKN= total Kjeldahl nitrogen

638 TP= total phosphorus.

639 **Table 2**

Dilution factor	ADPP				ADMW			
	5x	3x	1.5x	10x	7x	3.5x	2x	1x
Ammonium-N	70±10	115±15	230±35	84±10	120±20	240±40	420±65	840±130
Phosphate-P	4.8±0.2	8±0.3	16±0.7	0.20±0.0	0.29±0.0	0.57±0.1	1.0±0.1	2.0±0.2
<i>C. vulgaris</i>	1.9±0.2	3.0±0.1	5.1±0.9	0.6±0.1	0.6±0.2	1.1±0.1	1.2±0.1	0.9±0.1
VSS (g L ⁻¹)								
<i>S. acuminatus</i>	6.1±3.1	6.2±2.3	9.4±1.1	0.8±0.1	0.9±0.1	1.7±0.1	2.2±0.1	2.1±0.2
VSS (g L ⁻¹)								

640

641 **Table 3**

Medium	Microalgae	Maximum biomass concentration (g L ⁻¹)	Carbohydrates (%)	Lipids (%)	Proteins (%)	Reference
ADPP	<i>Chlorella vulgaris</i>	2.91 ^{a)}	6.8	21.7	30.3	This study
ADPP	<i>Scenedesmus acuminatus</i>	8.22 ^{a)}	60.5	19.9	24.3	This study
ADMW	<i>Chlorella vulgaris</i>	2.02 ^{a)}	6.3	23.0	41.8	This study
ADMW	<i>Scenedesmus acuminatus</i>	2.92 ^{a)}	44.3	35.9	28.0	This study
Anaerobic digested poultry litter	<i>Scenedesmus bijuga</i>	0.38	22.9	9.5	39.0	Singh et al. (2011)
Human urine	<i>Chlorella sorokiniana</i>	9.3	n.a. ^{b)}	n.a.	n.a.	Tuantet et al. (2014)
Anaerobic digested municipal wastewater	<i>Chlorella pyrenoidosa</i>	1.97	13.9	10.9	60.7	Tan et al. (2015)
Anaerobic treated Piggery wastewater	<i>Chlorella vulgaris</i>	3.24	n.a.	32	n.a.	Marjakangas et al. (2015)
Swine manure	<i>Chlorella vulgaris</i> , <i>Scenedesmus obliquus</i> and <i>Chlamydomonas reinhardtii</i>	1.25	50	20	25	Molinuevo-Salces et al. (2016)
Anaerobic digested sewage	<i>Scenedesmus sp.</i> and/or <i>Chlorella sp.</i>	0.42	n.a.	n.a.	n.a.	Viruela et al. (2016)
Tris–acetate–phosphate medium	<i>Chlamydomonas reinhardtii</i> UTEX 90	12.4	59.7	n.a.	9.2	Choi et al. (2010)
Modified Basal Medium	<i>Chlorella vulgaris</i> FSP-E	7.22	50.4	n.a.	n.a.	Ho et al. (2013)

642 Note: This table gives an indication of the range of microalgal biomass production and cell compositions obtained in
643 various studies but the given values cannot be explicitly compared as the studies have been conducted using different
644 growth conditions (photobioreactor design, light intensity, CO₂ addition, nutrient concentration etc.).

645 ^{a)} Only biomass values from Experiment II are reported, as biomass composition was not measured in Experiment I

646 ^{b)} n.a.=data not available